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# COMPOUNDING TECHNIQUES FOR ABSORBENT DECONTAMINANTS

AD893613

Final Report (August 1970 - November 1971)

by

Dewey P. Parks

January 1972





DEPARTMENT OF THE ARMY

EDGEWOOD ARSENAL

Development and Engineering Directorate

Edgewood Arsenal, Maryland 21010

Contract Number DAAA15-70-C-0362

Brunswick Corporation Technical Products Division Marion, Virginia 24354



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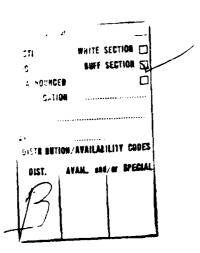
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Final Report.

(Aug 1970 - November 1971)

by

Dewey P./Parks Robert L./Copeland

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DEPARTMENT OF THE ARMY EDGEWOOD ARSENAL

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Brunswick Corporation Technical Products Division Marion, Virginia 24354

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#### **FOREWORD**

The work described in this report was authorized under Contract DAAA15-70-C-0362, Compounding Techniques for Absorbent Decontaminants. This work was started in August 1970 and completed in November 1971.

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#### **ACKNOWLEDGMENTS**

Acknowledgment for technical assistance to Mr. Harold Cook, Dr. Charles Greene, and Mr. Robert Hurley.

#### DIGEST

The objective of the program was to develop decontaminating systems for persistent chemical agents using micronized carbon. These systems must be effective in absorbing chemical agents and designed to the following goals.

- Act rapidly over a wide temperature range
- Be non-toxic and remain stable
- Not damage material and equipment on contact
- Be easily and rapidly applied to vehicular equipment, clothing and ancillary equipment.

The method of study was to select key ingredients, i.e., activated carbons, thixotropic agents, dispersants, pigments and solvent/antifreeze and formulate a system containing a minimum of 25% active carbon. It should be easily applied by spraying to a coverage of 4 mg/cm² and remain stable (not settle during static storage of at least two years). Key methods of investigation included evaluation of mixing techniques, effects of various thixotropes and dispersant on viscosities and stability and the evaluation of spray equipment for optimization of techniques as well as equipment. In addition, studies were conducted whereby dry formulation of the same key ingredients were formulated using high shear dry mixers. These compounds were tested for uniformity, adhesion to woven surfaces and effective coverages in the 4 mg/cm² range.

The results of these studies show that formulations containing approximately 35% active carbon can be easily sprayed to the desired coverage and will remain stable for the desired two year period. All of the program goals outlined above were met or exceeded by this study. Results also show dry formulations can be prepared by a special screened milling process to give the desired uniformity, color and adhesion.

It is concluded that in selecting the optimum ingredients to prepare a stable, sprayable thixotrope that will meet all of the Edgewood requirements, the following materials have shown to be superior: coal, petroleum, coconut and wood based activated carbons are suitable as agent absorbents; however, the coal and petroleum-based appear slightly superior. Thixotropes appear to be limited to the inorganic type with bentonite showing superior thixotropic properties. Dispersants are effective in lowering viscosities with the sodium salts of polymerized substituted benzoid alkyl sulfonic acid being most effective. Color can be obtained with iron oxide and 1/2% sodium chromate or sodium silicate to inhibit rust. A homogenizer mixer will produce uniform mixtures of the wet-system and a special screen milling machine will prepare satisfactory dry formulations.

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# COMPOUNDING TECHNIQUES FOR ABSORBENT DECONTAMINANTS

#### INTRODUCTION

The objective of this program is to develop a universal decontaminating system for persistent chemical agents using micronized carbon. The decontaminating system must be effective in absorbing the chemical agents and is designed to the following goals:

- · Act rapidly over a wide temperature range
- · Be non-toxic
- · Not damage material and equipment on contact
- Be easily and rapidly applied to vehicular equipment, clothing and ancillary equipment.

This study was particularly directed toward the application of activated carbon to vehicular equipment by spraying and to clothing and small equipment by dusting or rubbing. The program was conducted in three phases; i.e., (A) Vehicular decontaminants in the form of a sprayable suspension, (B) Clothing and individual equipment decontaminants in the form of dry powders, and (C) Scale-up methods and equipment for large volume manufacture and dispensing.

At the direction of Edgewood Arsenal, priority was placed on the successful completion of Phases A and B and if time and money permitted, Phase C was to be investigated.

The work performed during this contract shows how the key ingredients - activated carbon, thixotropic agents, dispersants, pigments, and solvent/ antifreeze - are combined into a system to accomplish the objectives outlined above. Numerous experiments, which resulted in varying degrees of success at accomplishing the combined systems goal, are discussed in this final report.

#### II. PHASE A - VEHICULAR DECONTAMINATION

This decontaminant was formulated from active carbon, a dispersant, pigment to give an olive green color, a thixotrope, a corrosion inhibitor, alcohol for antifreeze and water. The system must contain a minimum of 25% active carbon, be easily applied by spraying to give a coating of 4 mg/cm², and remain stable (not settle) during static storage for at least two years.

#### A. Materials

To begin the investigation, candidate materials were selected for initial investigation. Based on previous research completed by Edgewood Arsenal and previous work by Brunswick Corporation, the following candidate materials were selected.

Activated Carbons - Carbons derived from wood, coal, petroleum coke and coconut shell were investigated. These particular carbons were selected on the basis of their gas vapor absorptive properties which are of utmost importance in this application. Previous research has shown the optimum particle size to be in the  $1-2\mu$  range with any remaining particles being less than  $20\mu$ . The carbons evaluated in this program were as follows:

Carbon	Particle Size as Supplied	CCL <sub>4</sub> Activity	_pH_	Surface Area, Sq. Meters/g.
Coal Base				
CWS* (Pittsburgh Carbon Co.)	1-2 <sub>µ</sub>	65%	10.0	1000-1100
Coconut Shell Base				
Type UU (Barnebey-Cheney	50 x 200 )	100%	10.4	1400-1600
Petroleum Coke				
Type ACC (Union Carbide)	Granular	63%	10.4	980-1080
Wood Base				
DARCO KB (Atlas Chemical *Supplied b	1-2μ Co.) y Edgewood Arser	84% na1	5.2	600-700

Prior to formulating any carbon suspensions, particle sizes of the petroleum coke and coconut shell based were reduced to the desired 1-2 $\mu$  range. This was done by pulverizing with a hammer mill to reduce the particle size to approximately  $40\mu$ . The additional reduction was completed by ball milling for 4-1/2 hours. Particle sizes were then measured by a Sub-Sieve Sizer. The average particle size of each of the two sized carbons was in the 1-2 $\mu$  range.

Thixotropic Agents - By incorporating a thixotropic agent into the system, the viscosity of the carbon suspensions can be adjusted high enough to prevent settling of the carbon particles during static storage, yet remain fluid enough for spray application when shear is applied. Based on previous Brunswick development work with thixotropic agents in liquid propellants, plus earlier research by Edgewood Arsenal, the following candidate thickening agents were selected for study.

# Thixotropic Agent Carboxy Vinyl Polymer System (water soluble)

Type/Manufacturer
Organic, Carbopol R/
B. F. Goodrich Co.

Thixotropic Agent

Microcrystalline Silica

Micromesh Montmorillonite

Resin Grade Asbestos

Pyrogenic (Fumed) Silica

Microcrystalline Nylon

Type/Manufacturer

Inorganic, Avibest C/

FMC Corp.

Inorganic, Bentonite/ Van Horn Metz Co.

Inorganic, Calidria

RG-244/Union Carbide Co.

Inorganic, Aerosil COK-84/

DeGussa, Inc.

Organic, Aviamide 6-P Nylon/

FMC Corp.

<u>Dispersants</u> - To aid in obtaining low viscosities and to permit maximum percent carbon loading, dispersing agents were evaluated. With the majority of the carbons under investigation being basic, (pH  $\sim$  10) solid, anionic dispersants were used to effectively separate each of the carbon particles which increased the stability of the mixture. Those investigated were:

Dispersant

Polymerized Salt of Alkyl Naphthalene Sulfonic Acid

Partially Desulfonated Sodium Liquosulfonate

Sodium Salts of Polymerized Substituted Benzoid Alkyl Sulfonic Acid

Water Miscible Polymer

Trade Name/Manufacturer

DAXAD 11 - W. R. Grace Co.

Marasperse CB - American

Can Company

DARVAN No. 2 - R. T. Vanderbilt Company

Nopcosant K - Nopco Chemical Company

The effects of adding each of the dispersing agents to the carbon suspensions are discussed in the experimentation section.

<u>Pigments</u> - To produce an olive green color, pigments were selected and evaluated on the basis of "coloring power", i.e., the pigment which at the lowest weight percentage gave an olive green color.

Pigment

Iron Oxide

Phthalocyanine Green

Trade Name/Manufacturer

Mapico 1100 Yellow/Columbian

Carbon Company

Color No. W-6012/Harshaw

Chemical Company

Pigment

Cadmium Yellow

Cadmium Yellow

Cadmium Orange

Cadmium Sulfide

Trade Name/Manufacturer

Color No. 1489/Harshaw Chemical Company

Color No. AZO W-1215/ Harshaw Chemical Company

Color No. 1510/Harshaw

Chemical Company

Cadmium Yellow/Harshaw Chemical Company

<u>Corrosion Inhibitor</u> - To inhibit rust and corrosion following application of the decontaminant to a surface, the following materials were selected and evaluated.

Type

Sodium Chromate (Na<sub>2</sub>CrO<sub>4</sub>)

Sodium Silicate (Na<sub>2</sub>SiO<sub>3</sub>)

Source

Fisher Scientific

Fisher Scientific

Solvent-Antifreeze - As a carrier and antifreeze, the following was used.

Water - Demineralized

60 parts by volume

Methyl Alcohol

40 parts by volume

#### B. Mixing and Testing Equipment

Different pieces of equipment were selected and tested for efficiency and ease of mixing. Each piece of equipment was tested by mixing a formulation for given time intervals, then measuring the viscosity, followed by visual inspection and uniformity. The equipment tested is as follows:

Ball Mill - Formulations were ball milled a minimum of 48 hours using a 2 liter jar with approximately 1 pint of 1/2" diameter balls. The viscosity and stability data obtained from these experiments were used for comparison both to work done by Edgewood Arsenal and to the mixing efficiency of the other types of equipment.

Homogenizer Mixer - Figure I shows the Gifford-Wood, Model L-1 Homogenizer. It is characterized by a fixed clearance between a turbine and a stator head. The skewed turbine develops a pressure differential between the bottom of the turbine and the surface of the slurry. Unmixed material is continuously drawn from the bottom and forced through restricted openings in the stator striking the deflector

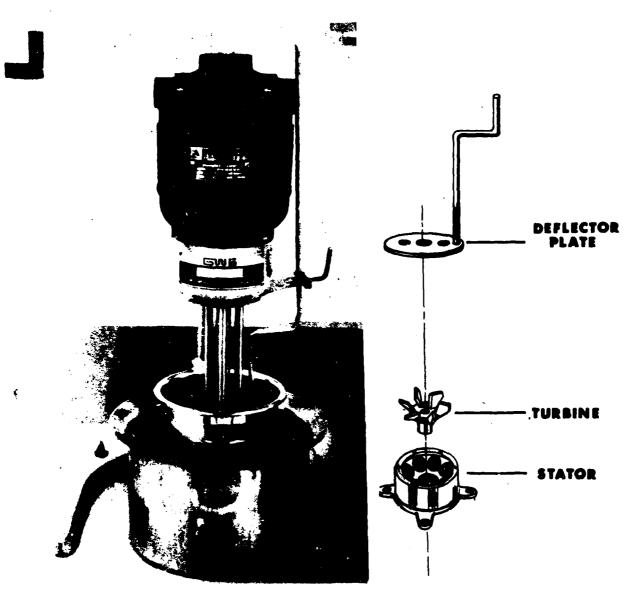


FIGURE 1 -

MIXER HEAD DETAILS

# L-1 HOMOGENIZER MIXER

WITH MIXING VESSEL AND ICE BATH

plate. Models are available with batch capacity of 2000 gallons and pipeline (continuous) models capable of 2000 gallons per minute.

Cowles Dissolver - A conventional high shear mixer designed with a drive shaft extending to the base of the mixing vessel. A circular impeller having an arrangement of blades provide intensive mixing. The agitator RPM equals the motor RPM.

<u>High Shear Blender</u> - For short duration mixing and small experimental sample batches of active carbon slurries, a conventional "Waring" type blender was used for convenience. This type mixer was primarily used in testing the water soluble polymer thixotropes.

Viscosity Measurements - The viscosity of the mixtures prepared was measured with a Brookfield Syno-lectric Viscometer fitted with a Helipath Stand. This attachment is especially designed for non-Newtonian viscosity measurements, moving the spindle in a sinusoidal path to avoid tracking and the attendant decrease in shear stress. Result, have been very consistent over a range of 100 to 60,000 centipoise depending upon shear rate, i.e., spindle speed.

Settling Tests - A centrifuge was set up to test carbon slurries for settling. Based on previous work with thixotropes, it was determined that centrifuging a loaded thixotropic material at 6 g's for 5 minutes simulates storage of the material for 2 years. A centrifuge having a swing arm radius of 1.1275 feet turning at 125 RPM results in the required 6 g loading. Test Tube samples of the slurry were placed in the holder and tested for the required 5 minutes. From the behavior of the slurry, simulated storage can be determined in a short period of time.

<u>Spray Equipment</u> - An apparatus using nitrogen gas as an expellant was used in experimental sprayings. A measured average pressure of 200 psi was used simulating the standard nitrogen cartridges used in present U.S. Army spraying equipment.

To allow a variety of nozzles to be investigated, an adaptor was machined to allow the sprayer to accept certain types of commercially available nozzles. Nozzles supplied by the Grayco and DeVilbiss Companies were evaluated.

Aluminum Test Panels - Two 24" x 24" aluminum test panels were painted with 1 mil of chromate primer and 1 mil of lusterless, 0G, Alkyd Lacquer, as required by the Edgewood specification. Test tabs, one square inch, were used to determine coverage.

#### C. Formulation and Experimentation

#### 1. Organic Polymer Thixotropes

Data and experience obtained from an earlier thixotropic study was used as a starting point to begin work on this program. This earlier project involved the development of a thixotropic propellant that would suspend particles in the low micron range and would remain completely stable and uniform over a two year period at static storage. This was successfully formulated by a thixotrope with an apparent viscosity of 20,000 centipoise at a shear rate of 1 sec-1 and 200 centipoise at a shear rate of 200 sec-1. This was accomplished using a water soluble resin to form a carboxy vinyl polymer system. Application also required that the material be forced through a small orifice very similar to spraying. Thus a high degree of thixotropy was necessary.

With this data in mind, the initial experiments were made to determine the effects of pretreatment of material, sequence of addition and method, intensity and duration of mixing on the resulting mixture.

Two typical formulations were used in this initial work; one composed of carbon, microcrystalline asbestos, pigment, sodium chromate corrosion inhibitor and carrier (alcohol-water); the second composed of carbon, Carbopol 934 vinyl polymer thixotrope, pigment, sodium chromate and carrier. In some formulations, traces of wetting agent, and triethanolamine as a neutralizer, were used.

A variation in composition, treatment and process was tried. Depending upon the formulation under test, the following general steps apply.

#### Step One - Addition of Thixotropic Agents

When formulating a thixotrope using the polymeric gelling agent, it is necessary to dissolve the powder into the carrier at high shear such as a "Waring" blender will produce. Attempts to add this gelling agent to the combined carbon-pigment slurry results in undissolved particles of Carbopol and inconsistent mixing. On the other hand, Avibest C, microcrystalline asbestos, was found to dispense more evenly and form better mixtures when added to the combined carbon-pigment mixture than when blended into either independently.

#### Step Two - Addition of Carbon and Pigment to the Thixotrope

Best results have been accomplished by thoroughly mixing the carbon and pigment together before adding to the carrier. A number of methods were tried including (1) screening the two components

together through a 40 mesh screen, (2) ball milling for 15 to 30 minutes, and (3) hand mixing with a spatula. Hygroscopic properties of the pigment limit the effect of ball milling as the dry material tends to "pack" causing the ineffective mixing. Either screening or hand mixing thoroughly was proven satisfactory.

#### Step Three - Required Mixing to Form Uniform Slurry

Tests were conducted on standard impeller mixers, high shear Welax types, Cowles dissolvers, and Waring blender type mixers. It was found that short duration (less than I hour) high shear mixing, such as that experienced in the Cowles dissolver or Welax mixer forms more stable suspensions than longer mixing at any shear rate. To establish a breakdown point caused by excessive shear mixing, tests have been conducted for several hours resulting in both Carbopol and Avibest C suspensions having been degraded by excessive mixing.

It was found that the consistency of the carbon slurries varied considerably with the type carbon used, i.e., the finer particle sizes formed a very thick paste. With the smaller particle sized carbons, additional carrier was required to keep the mixture sufficiently fluid to complete the formulation. The CWS carbon  $(1-2\mu \text{ range})$  wet out easily without additional carrier.

Results obtained in the preliminary evaluation indicated the Carbopol polymer system to be both easier to formulate and more stable after short mixing times than was the Avibest C. Considering ease of manufacturing as a primary objective, it was desired to concentrate efforts in preparing a stable thixotropic slurry using the Carbopol system. Avibest C was later withdrawn from the market and was not available for further evaluation.

#### Step Four - Stabilization of Carbon/Carbopol Thixotropes

Carbopol water-soluble resins are carboxy vinyl polymers of extremely high molecular weight supplied as dry fluffy powders in acid form. This material requires neutralization to develop optimum properties. The solutions gel at a pH of 7-10 and exhibit the following properties.

- Thickening efficiency very small amounts (less than 1/2%) are often required to give the required viscosity.
- Stability relatively unaffected by temperature and is not subject to hydrolysis or oxidation.
- Safe and Resistant used in drugs and cosmetic applications and is not attacked by or will not support mold growth.
- Versatile and Uniform used in many applications and affords reproducibility.

Carbopol gelling agent is available in three concentration forms, i.e., 934, 940 and 941.

The following tests were performed under identical conditions for comparison. All gels were prepared in a Waring type blender with shear mixing constant at 2 minutes.

Test 1 - 300 ML Solvent (40 methanol/60 water)

l g <u>Carbopol 934</u>

5 drops triethanolamine

Viscosity at 1 sec<sup>-1</sup> and 77°F - 7,000 cps

Test 2 - 300 ML Solvent

1 g Carbopol 940

5 drops triethanolamine

Viscosity at 1 sec and 77°F - 16,000 cps

Test 3 - 300 ML Solvent

1 g Carbopol 941

5 drops triethanolamine

Viscosity at 1 sec and 77°F - 1,000 cps

Because Carbopol 934 exhibits the highest degree of thixotropy (Figure 2) which is advantageous in spray applications, it was selected to develop a stable thixotropic suspension with activated carbon. A typical formulation for this phase of work contained:

CWS Carbon	180 g
Carbopol 934	3 g
1100 Yellow	30 g
Sodium Chromate	3 g
Carrier	950 ML (60/40 water/methanol)
Triethanolamine	3 a

and, in some experiments

HCL 1-3 drops

When activated carbon is chemically basic, mixing the Carbopol-Carbon slurry was hampered by premature gelling of the Carbopol. To prevent this, one of two methods can be employed. First, the carbon slurry was neutralized with hydrochloric acid permitting the blending of the formulation followed by the addition of more triethanolamine which renders the mixture basic again. Results of this technique were somewhat erratic, possibly due to the

absorptivity of the carbon which tends to delay the neutralization of the carbon slurry both with acid and again with triethanolamine. Second, the Carbopol was added to the carrier prior to the addition of the carbon and pigment. After high shear mixing to a uniform slurry, the neutralizer was added to form the gel. This second method proved to be the more effective.

After formulating a variety of suspensions using different concentrations of gelling agents and mixing techniques, the stability study began. Stability of mixtures prepared was checked by static storage for up to eight weeks and by centrifugal tests. As described in the equipment section, centrifugal tests at 6 g's for 5 minutes is roughly equivalent to two years static storage. Accordingly, this test has been applied here. Although static storage time is relatively short, the results are consistent, i.e., those mixtures failing the centrifugal tests have shown settling in 1-6 weeks storage.

The causes and effects of syneresis was briefly investigated. After 18-24 hours storage, unstable and even some apparently stable gels accumulate small quantities of solvent (exudate) on the surface. Attemps were made with this exudate either to prevent its occurring or to possibly affect its recombination.

After numerous experiments, it was discovered that the corrosive inhibitor, sodium chromate, had adverse effects on the carboxy vinyl polymer. By omitting this particular corrosive inhibitor the problem of syneresis was eliminated.

After the formation of Carbopol 934/carbon thixotropes with an apparent visocity in the 20,000 centipoise range, selected samples were placed in sealed glass containers to test the effects of static storage. After undisturbed storage ranging from 10 to 30 days, viscosity measurements showed a decrease in those samples selected for tests. This unexpected drop in viscosity in most cases resulted in light or "soft" settling of some carbon particles.

Tables I and II lists formulations of Carbopol 934 and 941 selected for static storage tests and the viscosity changes.

Although reconstitution can be easily accomplished by one or two snakes of the container, it is felt that a completely stable slurry could be obtained.

In selecting the Carbopol 934 to begin the investigation, consideration was given to the degree of thixotropy at various shear rates as exhibited in Figure No. 2. This chart gives the viscosity at different shear rates and shows Carbopol 934 to exhibit a greater viscosity drop as the shear increases. This, of course, would

result in a more sprayable thixotrope. As shown by the chart, Carbopol 941 is less affected by increases in shear, thus somewhat less attractive for spray applications, but gives a more stable thixotrope at lower viscosity.

Applying the same techniques as developed for Carbopol 934, formulations were made using Carbopol 941 as the gelling agent. Table II gives results of several formulations using Carbopol 941. As before, various concentrations were stored in sealed glass containers to test the effect of static storage. As this table shows, relatively no changes in viscosity or pH were measured over the thirty day storage period.

Due to the fact that the Carbopol 941 thixotropes are somewhat harder to spray, efforts to develop the lowest possible stable viscosity were pursued. Slurries with measured viscosities of 5,000 centipoise show stability at static storage for 30 days.

#### Results of Organic Polymer Systems as Thickening Agents

After stabilized mixtures of active carbon, pigment, corrosion inhibitor and water-alcohol, with the carboxy vinyl polymer system as the thixotropic agent, had been successfully developed, samples of the carbon/Carbopol suspensions were submitted to Edgewood for gas absorptive tests.

Although this particular system satisfied all the requirements of the Edgewood specification related to settling, permeability, sprayability, etc., results of the agent tests performed at Edgewood showed that the film forming properties of the vinyl polymer gels adversely affect the absorptive properties of the active carbon. As this property of the carbon is essential, organic thixotropes of this type were eliminated from additional study.

A total of seventy-seven experiments were conducted in evaluation of the vinyl polymer thickening system; therefore, tabulation of experiments with the inorganic thixotropic agents will begin with number 78 in this report.

#### 2. Inorganic Thixotropes

#### a. General Outline of Investigation

Due to the infinite number of possible combinations of materials and mixing equipment, key combinations were selected as shown in Table III. The table represents a general scheme of procedure. Experiment 1X will serve to

TABLE I

# STATIC STORAGE TESTS OF CARBON/CARBOPOL 934 THIXOTROPES

<u>Formula</u>		<u>Procedure</u>
CWS Carbon	180 g	From Thixotrope,
Solvent	950 ml	Mix carbon/1100,
Carbopol 934	2.6 g	Blend into carrier
TEA	27 drops *47 drops	Shear

1100 Yellow

30 g

		•	1	STAB	ILITY, V	ISCOSITY,	CPS	
FORMULATION NUMBER	SHEAR TIME WELAX MIXER	рН	Imed. After Mix	After 16 hrs	After 10 days	After 20 days	Afte Reconsti	
C-1	32 min. @ 25 psi	6.9	21,800	22,700	12,000	12,000 soft settling	10,000	<u>рН</u> 7.2
C-2	32 min. 0 25 psi	6.4	26,000	23,000	17,000	17,000 soft settling	7,000	7.2
C-3	5 min. @ 45 psi 2 min. @ 40 psi 25 min. @ 25 psi	6.7	16,000	16,000	10,000	9,000 settling	3,000	7.2
C-4*	5 min. @ 45 psi 2 min. @ 40 psi 25 min. @ 25 psi	7.0	26,000 /	24,000	18,000	10,000 soft settling	10,000	7.3
C-5*	5 min. 0 45 psi 2 min. 0 40 psi 15 min. 0 25 psi	7.1	31,000	33,000	23,000	15,000 holding	15,000 holding	7.3
C-6*	5 min. 0 45 psi 2 min. 0 40 psi 25 min. 0 32 psi	7.1	24,000	20,000	17,000	10,000 holding	10,000 holding	7.2

TABLE II

STATIC STORAGE TEST OF CARBON/CARBOPOL 941 THIXOTROPES

Formula		Procedure
BPL Carbon	180 g	Carbon blend into carrier
Solvent	950 ml	Carbopol blend into carrier
Carbopol 941	(as shown)	Two mixed together
Neutralizer	(as shown)	Shear and neutralize
1100 Yellow	30 g	

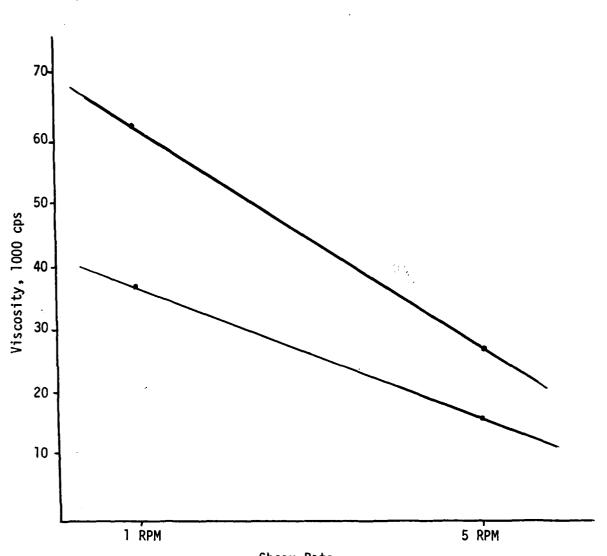
						STABILIT	Y, VIS	STABILITY, VISCOSITY & PH	& pH				
EXPERIMENT	CARBOPOL 941 &	IMMEDIATELY	ATELY	AFTER	ER	AFTER	2	AFTER	R	AFTER	:R	AFTER	E.R
NUMBER	NEUTRALIZER	AFTER	TER MIX	24	24 HRS.	48 HRS.	RS.	3 DAYS	۲S	5 DAYS	\YS	30 DAYS	١٧S
	•	cbs	Hd	cbs	Hd	sdo	Н	cbs	Hd	cbs	hd	sdo	Hd
C-7	1% & TEA	14,000	7.1	14,000	7.2	7.2 14,000	7.1	7.1 14,000 7.1 14,000	7.1	14,000	7.1	7.1 14,000	7.1
C-8	1% & TEA <sup>2</sup>	7,000	7.2	7.2 7,000	7.0	7,000	7.0	7.0 7,000 7.0 8,000 7.1	7.1	8,000	7.1	8,000	7.1
6-3	1% & DIISO <sup>3</sup>	12,000	7.0	7.0 12,000	6.9	12,000	6.9	6.9 12,000 6.9 12,500 6.0 12,500	0.9	12,500	6.9	6.9 12,500	6.9
C-10	.50% & TEA	7,500	7.2	7,500	7.3	7,500	7.2	7.3 7,500 7.2 7,500 7.2 7,000	7.2	7,000	7.2	7,000	7.2
C-11	.33% & TEA	000,9	7.3	000*9	7.3		7.2	5,500 7.2 5,500 7.2 5,500	7.2	5,500	7.2	7.2 5,500	7.2
C-12	.15% & TEA	800	7.5	009	7.5				Settling	ing			1

1% Carbopol 941 based on solvent with equal amount of Triethanolamine.

NOTES:

 $^2$  Same quantities of Carbopol 941 and TEA with double amount of shear as No. C-7.

<sup>3</sup> Diisopropanolamine



Shear Rate
Brookfield Helipath Spindle Speed
FIGURE 2
VISCOSITY VS. SHEAR RATE IN
MEASURING THE DEGREE OF THIXOTROPY

evaluate types of mixing equipment for a preliminary selection based on uniformity, stability and ease of mixing of the slurries.

Experiments 2X, 3X, and 4X will serve to evaluate the basic stability of the carbon blacks. Formulas 5X, 6X, and 7X will show the effect of thixotroping agents on a particular carbon black. Experiments 8X, 9X, and 10X will aid in evaluating dispersants.

Generally, materials will be eliminated from the program based upon their performance when put into suspension, i.e. ease of mixing, stability, effect on viscosity, sprayability and more important, gas absorptive properties.

Viscosities are being taken with the Brookfield Viscometer, Model RVT, utilizing the Helipath attachment. Readings are also being taken with a standard #4 spindle at 10 and 20 rpm. The viscometer is allowed to stabilize for 10 revolutions before readings are taken.

Formulations are being stored as Parts A and B. Part A is being observed for stability at undisturbed storage. Part B is being reconstituted prior to checking the viscosity after 1, 7, 14, 30 and 90 days.

#### b. Selection of Optimum Mixing Equipment with a Standard Formulation

To measure the mixing efficiency of the different pieces of equipment, a standard formulation was selected. The formulation was as follows:

Ingredient	% Formula Wt.	Actual Wt.
CWS Carbon	25.0	300 g
Bentonite	.5	6 g
DAXAD 11	1.0	12 g
1100 Yellow Pigment	5.0	60 g
Sodium Chromate	.5	6 g
Methanol-Water	68.0	756 ml

Slurries were prepared by mixing for 30, 60, 90, 120 and 180 minute intervals using the nomogenizer and Cowles Dissolver. Friction-heating resulted in the need to utilize an ice bath to maintain a constant temperature below 70°F. Tables IV and V give results of these preparations. Slurries were also prepared by ball milling for 48 hours. These results are shown in Table VI.

TABLE III
PREPARATION OF CARBON SUSPENSIONS

TYPICAL EXPE	RIMENT	1 X	2X	ЗХ	4X	5X	6X	7X	8X	9X	10X
Based on 100 (% Solvent = Formula Weig	% by Weight 100% - % ht)										
Carbon	BPL (CWS)	25				25	25	25	25	25	25
	UU		25								
}	ACC	$\Box$		25							
	KC				25						
Thixotrope	Bentonite	.5	.5	.5	.5	.5	.5	.5			
	RG-244								.5		
Ì	COK-84.										
	Aviamide-6-P Nyl	on									
Dispersants	DAXAD 11	1	ון ו	7	1				ו	ו	1
	Marasperse CB					1					
Ì	Darvan No. 2						1				
ł	Nopcosant K							1			
Pigments	1100 Yellow	5	5	5	5	5	5	5	5	5	5
	Phthalocyanine Green										
1	Cadmium Yellow	<del>                                     </del>									
Corrosive Inhibitor	Sodium Chromate	.5	.5	.5	.5	.5	.5	.5	.5	.5	.5
	Sodium Silicate										

As shown by Tables IV and V, after 60 minute mixing time the homogenizer consistently gave slurries with higher viscosities than does the Cowles dissolver and more closely approaches the uniformity of those slurries prepared by ball milling (Table VI).

As each of the tables show, the viscosity of most formulations increases during storage. The reason for this increase is discussed later in this report. At this point, two possible reasons are that (1) during mixing only a small portion of the absorptive power of the carbon may be taken up by the solvent. During storage each particle may continue to absorb the solvent thus increasing the viscosity. Second, the fact that the slurries subjected to the least amount of mixing had the greatest increase in viscosity, it could be that insufficient mixing has produced a poorly structured bentonite lattice. During storage this weak lattice tends to collapse causing viscosity increases.

After evaluating the three different mixing techniques shown in Tables IV, V, and VI, the homogenizer type mixer was found to be superior from the standpoint of uniformity and ease of mixing. Therefore, it was selected as the mixing technique to be used throughout the remaining portions of the program.

#### c. Evaluation of the Different Based Carbons with the Key Ingredients

#### (1) CWS Carbon - Coal Based

The coal based activated carbon used in this evaluation was manufactured by the Pittsburgh Activated Carbon Company. The carbon supplied to Brunswick by Edgewood Arsenal had an average particle size of 1.5  $\mu$  and a pH value of 10.0 in aqueous solution. The surface area measured 1000-1100 sq. meters/gram with a CCL  $_{\!A}$  activity of 65%.

The different thixotropic and dispensing agents, shown in Section II-A, were first evaluated for effects on aqueous slurries of CWS activated carbon. Formulations were prepared with each thixotrope, i.e., bentonite, asbestos, pyrogenic silica and microcrystalline nylon, and are shown in Table VII.

Experiments 79, 83, 87, and 87-A show effects of each of the thixotropes when using Darvan No. I as the dispersing agent. As this series of experiments show, bentonite was the most efficient thixotropic agent in that it gave the highest, most stable viscosity. Experiments 115, 116, 117 and 118 were performed under the same condition substituting DAXAD II as the dispersant. Results again show bentonite to be the most efficient thixotropic agent by giving the highest viscosity with the other additives being held constant.

TABLE IV

CARBON SUSPENSION PREPARED WITH THE L-1 HOMOGENIZER

Formula	Formulation No.	1-78	1-79	1-80	1-81	1-92
Mixing	Mixing Time, Minutes	After 30	After 60	After 90	After 120	After 180
IMED.	Helipath <sup>(1)</sup>	12,000	6,000	8,000	11,000	11,000
AFTER MTV	#4* @ 10 RPM(2)	000,6	6,800	6,000	8,400	8,200
<b>41</b> E	#4 @ 20 RPM	5,100	3,400	3,100	4,100	4,150
AFTER	Helipath	15,000	12,000	10,000	10,000	11,000
24	#4 @ 10 RPM	14,000	000*6	7,600	7,500	8,700
CADORS	#4 @ 20 RPM	7,500	4,700	3,900	3,800	4,200
AFTER	Helipath	16,500	000*91	13,000	15,000	14,000
7	#4 @ 10 RPM	15,000	12,800	10 <b>,</b> 800	10,000	12,000
2	#4 @ 20 RPM	09,9	6,200	5,450	5,450	5,750
Solvent	Solvent Content, %	58.7	63.0	29.0	61.3	58.2
픱		10.5	10.5	10.4	10.4	10.4

(1) Brookfield Viscometer Model RVT with special Helipath attachment for measuring thixotropic materials

(2) With Standard #4 Spindle TABLE V

CARBON SUSPENSIONS PREPARED WITH A COWLES DISSOLVER

1						
Formula	Formulation No.	1-84	1-84	1-85	<u>ī</u> -93	1-94
Mixing	Mixing Time, Minutes	After 30	After 60	After 90	After 120	After 180
IMEL.	Helipath	4	5,000	4,000	7,800	7,000
AFTEK MIY	#4 @ 10 RPM	unmixed	4,800	3,900	9,000	5,500
<b>4</b> 1 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2 2	#4 @ 20 RPM		2,500	2,000	3,000	2,750
AFTER	Helipath	Α.	7,100	6,250	7,900	7,000
24 uniibe	#4 @ 1 C RPM	Unmixed	5,000	4,900	7,000	000*9
CADOLL	#4 @ 20 RPM		2,700	2,900	3,500	5,050
AFTER	Helipath		000,6	8,000	12,000	10,000
7	#4 @ 10 RPM		2,700	7,600	9,700	8,000
2	#4 @ 20 RPM		3,100	3,900	4,850	4,000
Solvent	Solvent Content, %		58.7	59.8	61.2	60.4
五			10.3	10.3	10.4	10.3

TABLE VI

CARBON SUSFENSIONS PREPARED WITH A BALL MILL

Formulation No.	tion No.	1-91	1-82	1-86
Mixing 1	Mixing Time, Hours	48	48	48
IMED.	Helipath	25,000	14,000	17,000
AFTER MIX	#4 @ 10 RPM	19,800	12,300	15,600
<b>X</b>	#4 @ 20 RPM	10,300	7,200	8,400
AFTER	Helipath	25,000	14,000	17,000
24 HOLIBS	#4 @ 10 RPM	19,200	12,400	13,800
	#4 @ 20 RPM	10,000	7,000	7,500
AFTER	Helipath	22,000	15,600	18,000
7 navs	#4 @ 10 RPM	18,600	14,000	16,300
2	#4 @ 20 RPM	4,800	8,000	8,450
Solvent	Solvent Content, %	27.73	57.3	57.2
Ηd		10.4	10.7	6.7

It was concluded from these two series of experiments that bentonite is a superior thixotropic agent to either asbestos, pyrogenic silica or microcrystalline nylon when using the CWS coal based carbon.

After selecting bentonite as the thixotrope agent for CWS carbon, different dispersing agents, DAXAD 11, Darvan No. 2, Marasperse CB, and Nopcosant K were evaluated for their effectiveness in lowering the viscosity. Experiments 115, 119, 120, and 121 (Table VIII) show initial evaluations of the dispersants. By assuming the lower viscosity indicates a better dispersion of carbon particles, experiment 120, using Marasperse CB dispersant, was selected for additional evaluation.

By analyzing experiments 134, 135, 137, and 141 (Table IX) it can be seen that carbon loadings up to 40% (Exp. 137) are possible using Marasperse CB, however, these slurries become glue-like in texture with a significant drop in viscosity during storage. Experiments 144, 145, and 147 were conducted to maximize carbon loading with a more stable viscosity. Experiment 145 using DAXAD 11 gave both a carbon content of 31.7% and more stable viscosity during storage. Therefore, DAXAD 11 was chosen as the superior dispersant.

After selecting bentonite as the most efficient thixotrope and DAXAD 11 as the dispersing agent, the next step was to determine the optimum percent concentrations of DAXAD 11. This was done by conducting the experiments shown in Table X. The results are also shown charted in Figure 3. Experiments 115, 149, 150, and 151 were conducted with a 300 gram CWS carbon loading ( $\sim$ 25%) with 12, 24, 36, and 48 grams ( $\sim$ 1, 2, 3, & 4%) of DAXAD 11 dispersant.

Experiments 152, 145, 153, and 154 contained 395 grams (31%) carbon loading. As the results show, there is a significant difference in reaction of the DAXAD 11 to the percent carbon loadings. This data indicates optimum to be 2% DAXAD 11 dispersant with each carbon loading.

The next series of experiments were prepared to test the effect of corrosion inhibitors. Experiments 145, 172, and 176, shown in Table XI, give the resulting viscosities of suspension prepared with sodium chromate and sodium silicate inhibitors. Both Experiments 176 and 172, containing .48% and .96% sodium silicate inhibitor, show a drop in viscosity with eventual settling. Sodium silicate did show a slight increase in pH over the sodium chromate. Based on stability of the suspensions, sodium chromate is selected as the better corrosion inhibitor.

Experiments 145, 184, 185, 188, and 201, shown in Table XII, were conducted to evaluate the effect of various mixing times using the L-1 Laboratory Homogenizer. As the results show, each increased mixing time produced a higher viscosity, however no apparent stabilization of the viscosities was achieved. It was concluded that additional mixing time beyond thirty (30) minutes does not improve the stability of the CWS suspensions. The solvent content of Experiments 145 and 201 measured 55.8% and 55.5% respectively, therefore solvent evaporation during mixing did not produce the increased viscosities.

Various types of pigments were evaluated to produce an olive green color. Cadmium lithopone yellows, oranges and phthalocyanine green pigments supplied by Harshaw Chemical Company were added to CWS suspension on concentrations up to 6.3%. As Table XIII shows, Experiments 191 with the Azo yellow and 193 with the cadmium lithopone gave considerable increases in viscosity without the desired olive green color. A 6.3% concentration of phthalocyanine green remained black. The Mapico 1100 yellow, iron oxide, pigment did give the desired olive green at a 4.8% level, therefore was selected over the other pigments tested.

After making final selections of a thixotrope, dispersant, pigment and corrosion inhibitor for use with the CWS carbon, some adjustments were made in solvent content. With a carbon content of 31.60% and a solvent content of 60.71% the resulting viscosity was in the 25,000 centipoise range. As can be seen by Spray Test No. 12, the coverage over the test panel was in the 20 mg/cm² range indicating the viscosity was too high for effective spraying. Also the resulting spray gave a spattered, non-uniform coating again indicating the material to be thick. The solvent content was then increased to 63.03% (reducing the carbon to 29.59%) which resulted in a viscosity in the 12-14,000 centipoise range. Slurries in this viscosity range can be effectively sprayed.

A typical formulation for CWS carbon used both for testing sprayability and adhesion would be as follows:

Ingredient	Actual <u>Weight</u>	Percent Formula Wt.
Carbon: CWS Carbon	385 g	29.59
Thixotrope: Bentonite	6 g	. 46
Dispersant: DAXAD 11	24 g	1.84
Pigment: 1100 Yellow	60 g	4.61
Corrosion Inhibitor: Sodium Chrom	ate 6 g	.46
Solvent: (60/40 Water-Methanol)	820 m1	63.03
Mixing Time: Thirty (30) minutes		
L-1 Laboratory Homoge	enizer	
Typical Viscosity at 24 hours	14,000 c	ps Helipath
after mixing		ps #4 @ 10 RPM
•	5,500 c	ps #4 @ 20 RPM
pH Value	10.4	•
Carbon Particle Size	1-2 μ (a	vg.)

TABLE VII

	CWS _CAR	BON - THI	XOTROPE	EVALUAT	ION			<b></b>	T
FORMULATIO	N NO.	79	83	87	87-A	115	116	117	118
COMPOSITIO	N BY/WT.			Ac	tual Wt.				
Carbon	CWS - Coal Based Carbon	300 g	300 g	300 g	300 g	300 g	300 g	300 g	300 g
Thix	otrope (1) Bentonite	6 g				6 g			
<b>5.</b> *	(2) RG-244		6 g				6 g		-
	(3) сок-84			6 g				6 g	İ
	(4) Nylon-6				6 g				6 9
Disp	persant (1) DAXAD 11					12 g	12 g	12 g	12 g
	(2) Darvan #1	12 g	12 g	12 g	12 g				
	(3) Marasperse CB	<b></b>							
	(4) Nopcosant K								
Pigr	ment 1100 Yellow	60 g	60 g	60 g	60 g	60 g	60 g	60 g	60 g
Cori	rosive Inhibitor (1) Na <sub>2</sub> C 0,	6 g	6 g	6 g	6 g	6 g	6 g	6 g	6 g
	(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>								
Solvent, V	Water/Alcohol 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML
MIXING TE	CHNIQUE: Homogenizer, min.	60	60	60	60	30	30	30	30

## CHARACTERISTICS

Viscosi	ty, CP							r	
Imed.	Helipath "C"	9,000	2,000	3,000	1,000	7,000	1,800	3,000	1,500
After	#4 @ 10 RPM	6,800	1,900	2,800	500	5,700	1,100	2,440	1,000
Mix	#4 @ 20 RPM	3,400	1,050	1,500	300	2,875	575	1,325	500
After	Helipath "C"	12,000	2,800	4,000	500	10,000	2,000	4,000	2,500
24	#4 @ 10 RPM	9,000	2,200	3,600	200	7,900	1,200	3,350	1,900
Hours	#4 @ 20 RPM	4,700	1,100	1,900	150	4,000	600	1,800	950
After	Helipath "C"	16,000	3,600	6,700		14,000	2,500	6,500	3,000
7	#4 @ 10 RPM	12,000	2,900	5,600		13,700	1,600	5,000	2,100
Days	#4 @ 20 RPM	6,200	1,300	2,750		4,850	775	2,650	1,000
After	Helipath "C"	17,000	2,000	7,000	<u>ا</u> د	14,000	2,900	6,800	2,500
14	#4' 0 10 RPM	12,500	1,400	5,700	ded Thi	10,200	1,500	5,350	2,300
Days	#4 @ 20 RPM	8,150	750	2,800	Sar 80	5,200	800	2,900	1,175
• • •	Helipath "C"	16,800	3,700	8,000	Dis - T	14,000	2,000	7,000	2,900
After 30	#4 @ 10 RPM	13,000	2,100	5,800	1	11,300	1,100	5,000	2,150
Days	#4 @ 20 RPM	6.800	1.125	2,800		5,550	600	2,550	1,000
pH		10.5	10.3	10.2		9.7	9.5	9.9	9.8

MUTES:

TABLE VII

CWS CAR	BON - THI	XOTROPE	EVALUAT	ION	<del></del>		r	
FORMULATION NO.	79	83	87	87-A	115	116	117	118
COMPOSITION BY/WT.			Ac	tual Wt.				
Carbon CWS - Coal Based Carbon	300 g	300 g	300 g	300 g	300 g	300 g	300 g	300 g
Thixotrope (1) Bentonite	6 g				6 g			
(2) RG-244		6 g				6 g		-
(3) COK-84			6 g				6 g	.
(4) Nylon-6				6 g				6 9
Dispersant (1) DAXAD 11					12 3	12 g	12 g	12 g
(2) Darvan #1	12 g	12 g	12 g	12 g				
(3) Marasperse CB								
(4) Nopcosant K								
Piament 1100 Yellow	60 g	60 g	60 g	60 g	60 g	60 g	60 g	60 g
Corrosive Inhibitor (1) Na C O.	6 g	6 g	6 9	6 g	6 g	6 g	6 g	6 g
(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>								
Solvent, Water/Alcohol 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML
MIXING TECHNIQUE: Homogenizer, min.	60	60	60	60	30	30	30	30

## CHARACTERISTICS

Viscosi	ty, CP	···		,					
Imed.	Helipath "C"	9,000	2,000	3,000	1,000	7,000	1,800	3,000	1,500
After	#4 @ 10 RPM	6,800	1,900	2,800	500	5,700	1,100	2,440	1,000
Mix	#4 @ 20 RPM	3,400	1,050	1,500	300	2,875	575	1,325	500
After	Helipath "C"	12,000	2,800	4,000	500	10,000	2,000	4,000	2,500
24	#4 @ 10 RPM	9,000	2,200	3,600	200	7,900	1,200	3,350	1,900
Hours	#4 @ 20 RPM	4,700	1,100	1,900	150	4,000	600	1,800	950
After	Helipath "C"	16,000	3,600	6,700		14,000	2,500	6,500	3,000
7	#4 @ 10 RPM	12,000	2,900	5,600		13,700	1,600	5,000	2,100
Days	#4 @ 20 RPM	6,200	1,300	2,750		4,850	775	2,650	1,000
After	Helipath "C"	17,000	2,000	7,000		14,000	2,900	6,800	2,500
14	#4' @ 10 RPM	12,500	1,400	5,700	ded Thi	10,200	1,500	5,350	2,300
Days	#4 @ 20 RPM	8,150	750	2,800	ca 8	5,200	800	2,900	1,175
1.64	Helipath "C"	16,800	3,700	8,000	Dis - ∓	14,000	2,000	7,000	2,900
After 30	#4 @ 10 RPM	13,000	2,100	5,800	1	11,300	1,100	5,000	2,150
Days	#4 @ 20 RPM	6,800	1.125	2.800		5,550	600	2,550	1,000
pH		10.5	10.3	10.2		9.7	9.5	9.9	9.8

NUTES:

### TABLE VIII

FORMULATION NO.	115	119	120	121	 _	
COMPOSITION BY/WT.			Ac	tual Wt.		
Carbon CWS - Coal Based Carbon	300 g	300 g	300* €	300 g		
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g		
(2)						
(3)						
· (4)						
Dispersant (1) DAXAD 11	12 g					
(2) Darvan No. 2		12 g				
(3) Marasperse CB			12 g		 	
(4) Nopcosant K				12 g	 	
Pioment 1100 Yellow	60 g	60 g	60 g	60 g	 	
Corrosive Inhibitor (1) Na C O.	6 9	6 g	6 g	6 9		
(2)						
Solvent, Water/Alcohol 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML		
MIXING TECHNIQUE: Homogenizer, min.	30	30	30	30		

Viscos i	ty, CP					 <del></del>	<del>-</del>	
Imed.	Helipath "C"	7,000	3,500	1,100	11,000	·		·
After	#4 @ 10 RPM	5,700	2,200	650	9,600			
Mix	#4 @ 20 RPM	2,875	1,225	400	5,675			
After	Helipath "C"	10,000	1,500	1,000	9,400			
24	#4 @ 10 RPM	7,900	900	, 600	8,500			~
Hours	#4 @ 20 RPM	4,000	500	350	4,550			
After	Helipath "C"	14,000	1,000	1,800	7,500			
7	#4 @ 10 RPM	13,700	450	1,000	7,250			
Days	#4 @ 20 RPM	4,850	300	550	3,875			
After	Helipath "C"	14,000	1,000	1,800	7,300			
14	#4 @ 10 RPM	10,200	400	1,000	6,800			
Days	#4 @ 20 RPM	5,200	250	550	3,675			
	Helipath "C"	14,000		1,500	6,800			
After 30	#4 @ 10 RPM	11,3000	iscarde	d 750	6,000			
Days	#4 @ 20 RPM	5,550	oo Thii	425	3,325			
рН		9.7	9.5	9.6	9.8			

		CWS CAR	BON - DIS	SPERSANT	EVALUA	TION			r	
FORMULATION	N NO.		134	135	137	141	144	145	147	
COMPOSITION	N BY/WT.				Ac	tual Wt.	•			
Carbon	CWS - C	oal Based Carbon	425 g	450 g	500*g	450 g	430 g	395 g	325 g	
<u>Thix</u>	otrope (1)	Bentonite	6 g	6 g	6 g	9 g	6 g´	6 g	6 g	
۲.	(2) (3)									* * * Z
<b>0.</b> 2	(4)		10.10	21.	24.	24 g				<u>:</u>
עונע	ersant (1) (2)	Marasperse CB Darvan No. 2	12+12 g	24 g	24 g	24 9	24 g			
	<u>(3)</u> (4)	DAXAD 11 Nopçosant K						24 a	24 g	
Pion	ent	1100 Yellow	60 g	60 g	°60 g	60 g	60 g	60 g	60 g	
Corr	osive Inhib	itor (1) Na <sub>2</sub> C <sub>1</sub> O <sub>1</sub>	6 g	6 g	6 g	6 g	6 g	6 g	6 g	
Solvent, k	later/Alcoho	1 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	
MIXING TEC	CHNIQUE: Hor	mogenizer, min.	30+30	30	30	30	30	30	30	· :

# CHARACTERISTICS

Viscosity, CP		(34,000)		,					<b>-</b>
Imed. After Mix	Helipath "C"	10,000	6,000	15,000	15,000	14,500	16,500	11,000	·
	#4 0 10 RPM	5,400	2,800	6,300	6,000	10,250	13,650	10,300	
	#4 @ 20 RPM	3,350	1,900	4,750	3,950	6,350	6,650	5,450	
After 24 Hours	Helipath "C"	5,000	2,000	12,000	7,000	6,000	16,000	10,000	
	#4 @ 10 RPM	1.850	1,100	4,900	2,900	3.725	13,000	9,200	
	#4 @ 20 RPM	1,200	775	3,650	1,950	2,500	6,325	4,900	
After 7 Days	Helipath "C"	3,000	1.500	8,000	5,000	3,200	23,500	9,000	
	#4 @ 10 RPM	1.300	900	2.900	2,100	1.900	17,600	8,200	
	#4 @ 20 RPM	900	700	2,225	1,400	1,300	8,650	4,500	
After 14 Days	Helipath "C"	2,000	1.200	5.000	4,000	2.800	25.000	8,800	
	#4 @ 10 RPM	1,000	800	2,200	1,625	1,400	19,600	7,700	
	#4 9 20 RPM	675	600	1,700	1,125	950	9,800	4,200	
After 30 Days	Helipath "C"	1,000	900	3,000	2,000	2,000	28,000	8,000	
	#4 9 10 RPM	700.	600	2,000	1,150	1,200	22,000	6,300	
	#4 0 20 RPM	500	450	1,650	850	850	11,100	3,500	
рН	DECAME CLUE LIVE	10.1	10.6	10.1	10.2	9.6	10.0	10.0	

MOTES: \*MIXTURE BECAME GLUE-LIKE WITH 500 g CARBON -34-

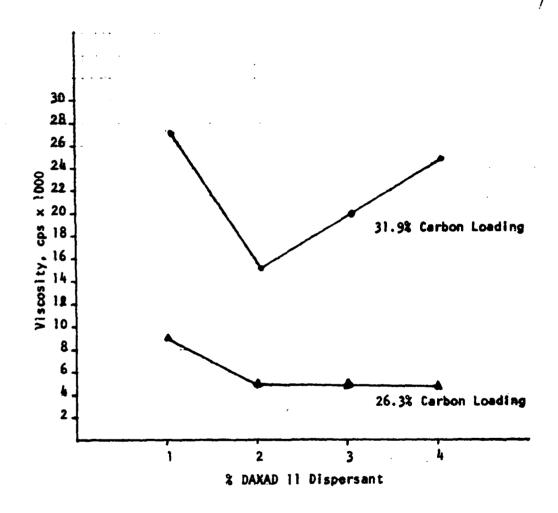


FIGURE 3 - EFFECT OF % DISPERSANT ON CWS CARBON SLURRIES

TABLE X

	CWS CARBON -	- PERCENT	DISPER	SANT EVA	LUATION		<b></b>	<del>y.</del> . <del>.</del>	, -
FORMULATION NO.		115	149	150	151	152	145	153	154
COMPOSITION BY/WT.				Ac	tual Wt				
Carbon CWS		300 g	300 g	300 g	300 g	395 g	395 g	395 g	395 g
<u>Thixotrope</u> (	]) Bentonite	6 g	6 g	6 g	6 g	6 g	6 g	6 g	6 g
<u></u>		ļ							JE.
	3)								
	4)	<b>_</b>							i
Dispersant (	1) DAXAD 11	12 g	24 g	36 g	48 g	12 g	24 9	36 g	48 9.
	2)	<del></del>							
(									
Pioment	1100 Yellow	60 g	60 g	60 g	60 g	60 g	60 g	60 g	60 g
Corrosive In	hibitor (1) Na C O	6 g	6 g	6 g	6 g	6 g	6 g	6 g	6 <u>c</u>
	2)								~~~
Solvent, Water/Ald	ohol 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	756ML
MIXING TECHNIQUE:	Homogenizer, min.	30	30	30	30	30	30	30	30

Viscosi	ty, CP		p						, <u>.</u>
Imed.	Helipath "C"	7,000	4,000	5,000	5,500	25,000	16,500	18,000	26,000
After	#4 @ 10 RPM	5,700	3,000	3,600	3,850	22,900	13,650	13,200	19,800
Mix	#4 @ 20 RPM	2,875	1,575	1,750	1,875	11,450	6,650	6,850	9,700
After	Helipath "C"	10,000	6,000	6,000	5,900	28,000	16,000	1	i
24	#4 @ 10 RPM	7,900	4,150	4,200	4,300	26,400	13,000		17,400
Hours	#4 @ 20 RPM	4,000	2,050	2,100	2,140	13,800	6,325	8,100	8,500
After 7	Helipath "C"						,		
	#4 @ 10 RPM								
Days	#4 @ 20 RPM								! <del> </del>
After	Helipath "C"								<del></del>
14	#4 @ 10 RPM		1	·					1
Days	#4 @ 20 RPM								
164	Helipath "C"								
After 30	#4 @ 10 RPM								1
Days	#4 @ 20 RPM								
ρΗ									

CWS CA	RBON - CO	RROSION	INHIBIT	TOR		 , -
FORMULATION NO.	145	176	172			 -
COMPOSITION BY/WT.			Ac	ctual Wt.		
Carbon CWS - Coal Based Carbon	395 g	395 g	395 g			
Thixotrope (1) Bentonite	6 g	6 g	6 g			 <u> </u>
(2)						 -
(3)						
. (4)						
Dispersant (1) DAXAD 11	24 g	24 g	24 g			
_ (2)						
_(3)						
(4)						
Pigment 1100 Yellow	60 g	60 g	60 g			
Corrosive Inhibitor (1) Na C O.	6 g					
(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>		6 g	12 g	·		
Solvent, Water/Alcohol 60/40 By Vol.	756 ml	756 ml	756 ml			
MIXING TECHNIQUE Homogenizer, minutes	30	30	30		Ì	<u> </u>

V.1 s cos 1	ity, CP			•	 	-	 
Imed.	Helipath "C"	16,500	4,000	11,000		· · ·	 
After	#4 @ 10 RPM	13,650	2.600	6,500			 
Mix	#4 @ 20 RPM	6,650	1,600	3,425			
After	Helipath "C"	16,000	1,000	1,000			
24	#4 @ 10 RPM	13,000	1,100	1,900			
Hours	#4 @ 20 RPM	6,325	700	1,100			
After	Helipath "C"	23,500	< 500	< 500			
7	#4 @ 10 RPM	17,600	√ 300	√ 300			 
Days	#4 @ 20 RPM	8,650	√ 250	√ 250			 
After	Helipath "C"	25,000					
14	#4 @ 10 RPM	19,600					
Days	#4 @ 20 RPM	9,800	c :-	hi ng			
	Helipath "C"	28,000	Th	ry t t 1			
After 30	#4 @ 10 RPM	22,000	S	Se			
Days	#4 @ 20 RPM	11,100					
рН		10.0	10.7	10.8			

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TABLE XII

CWS CA	RBON - M	MIXING T	IME STU	DY	<del></del> -	 4
FORMULATION NO.	145	184	185	188	201	 -
COMPOSITION BY/WT.			Ac	ctual Wt.		
Carbon CWS - Coal Based Carbon	395 g	395 g	395 g	395 g	395 g	
Thixotrope (1) Bentonite						 
(2)			L			 74
(3)						
(4)						<u> </u>
Dispersant (1) DAXAD 11	24 g	24 g	24 g	24 g	24 g	
(2)				<u> </u>		 
(3)			<u></u>	<b></b>		 
(4)			<u> </u>	ļi		 
Pigment 1100 Yellow	60 g	60 g	60 g	60 g	60 g	_
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 g	6 g	6 g	 _
(2)						
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756	٠756	756	
MIXING TECHNIQUE: Homogenizer, minutes	30	60	90	120	180	1:

CHA	DA	CT	CD	TCT	7	rc
LHA	NXA	LI	ĿΚ	12	ı	LS

Viscosi	ty, CP				·····		<del>_</del>	ı	,
Imed.	Helipath "C"	16,500	19,000	20,000	28,000	45,000			
After	#4 @ 10 RPM	13,650	14,300	15,300	20,200	28,000			•
Mix	#4 @ 20 RPM	6,650	7,100	7,625	9,900	14,400			
After	Helipath "C"	16,000	29,000	28,000	27,000	48,000			
24	#4 @ 10 RPM	13,000	19,800	18,000	19,000	32,200			
Hours	#4 @ 20 RPM	6,325	9,700	9,100	9,650	16,400	- 1		·
After	Helipath "C"	23,500	34,000	32,000	41,000	53,000			
7	#4 @ 10 RPM	17,600	25,100	23,200	29,400	35,600			
Days	#4 @ 20 RPM	8,650	12,500	12,000	15,100	18,000			· · · · · · · · · · · · · · · · · · ·
After	Helipath "C"	25,000	36,000	34,000	42,000	60,000			ļ
14	#4 @ 10 RPM	19,600	26,200	25,000	33,200	32,500			
Days	#4 0 20 RPM	9,800	12,800	12,200	16,800	19,000			
	Helipath "C"	28,000	34,000	34,000	45,000	57,000			
After 30	#4 @ 10 RPM	22,000	26,400	25,600	33,200	27,500			
Days	#4 @ 20 RPM	11,100	13,700	13,500	17,500	18,000			
рН		10.0	10.0	10.1	10.0	10.0			I.
Solv	vent Content, %	55.8	20			55.5			

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## TABLE XIII

CWS_CA	rbon -	PIGMENT	EVALUAT	ION		
FORMULATION NO.	145	191	192	193		
COMPOSITION BY/WT.			A	ctual Wt.		
Carbon CWS - Coal Based Carbon	395 g	395 g	395 g	395 g		
Thixotrope (1) Bentonite	6 g	<b>6</b> g	6 g	6 g		
(3)						
(4)					,	
. Pigment (1) 1100 Yellow	60 g					
(2) Azo Yellow		80 g				
(3) Pathalocyanine Gree	n*		80 g			
· (4) Cad Yellow/Cad Orang	2			56/5 g		
Dispersant DAXAD 11	24 g	24 g	24 g	24 g		
Corrosive Inhibitor (1) Na2Cr04	6 g	6 g	6 g	6 g		
(2)						
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756	756		
MIXING TECHNIQUE	30	30	30	30		

## CHARACTERISTICS

V1s cost	ity, CP		·	· · · · · · · · · · · · · · · · · · ·	<del></del>	<del></del>			
Imed.	Helipath "C"		16,500	42,000	3,500	46,000	 	<u> </u>	<u> </u>
After	#4 @ 10 RPM		13,600	20,400	1,200	29,800			
Mix	#4 @ 20 RPM		6,650	10,300	750	16,200			
After	Helipath "C"		16,000	1		/			
24	#4 @ 10 RPM		13,000						
Hours	#4 @ 20 RPM		6,325	1					
	-	Color,	Olive	Dark		Medium			
	-	Wet	Green	Green	Black	Green			
	<u>-</u>	Color.	Olive	Green		Dark			
		Dry	Green	Black	Black	Green			
	_								
	_								
							<del></del>		
pH		•							

\*Supplied by Harshaw Chemical in aqueous suspension -39-

#### (2) <u>Darco KB Carbon - Wood Based</u>

The wood based carbon is manufactured by the Atlas Chemical Company and is supplied with an average particle size of 1.2  $\mu$ . The pH value in aqueous solution is approximately 5.2 with a surface area of 600-700 square meters/gram and a CCL<sub> $\Lambda$ </sub> activity of 84%.

In evaluating Darco KB carbon, the same general plan of experimentation was used as with the CWS carbon. Experiments 95, 96, 97, 103, 104, and 106, shown on Table XIV, gives results when the carbon is combined with each of the thixotropic agents. After solvent adjustment was made (Exp. 95, 96, and 97) to keep the slurry sufficiently fluid to mix, slurries were prepared with each of the thixotropes using DAXAD 11 as the dispersant. By analyzing Experiments 97, 103, 104, and 106, it can be concluded that bentonite was the most efficient thixotropic agent in that it gave the highest workable viscosity. Although RG-244 asbestos, shown in Experiment 103, gave a very high viscosity, in order to prepare a mixable slurry it would be necessary to (1) lower the carbon content below 24%, (2) lower the thixotrope below 1/2%, which would not be a sufficient amount to hold the carbon particles in suspension, or (3) raise the solvent content, all of which are undesirable.

It was concluded from this series of experiments that bentonite is the superior thixotropic agent with Darco KB wood based carbon.

In evaluating dispersants with the Darco KB-bentonite system, slurries were prepared as shown in Table XV. It can be seen that Darvan No. 2 give the lowest viscosity, indicating the best dispersion of carbon particles. Experiment 148 was conducted using a cationic dispersant, Ammonyx 856, but the data shows the anionic dispersants gave a lower viscosity indicating better dispersion. Darven No. 2 dispersant was selected for further evaluation.

Table XVI shows results of increasing the carbon content of the Darco KB-bentonite system and the effect on viscosities. Experiment 143 gave the maximum loading at 25.4% carbon with the lowest viscosity. This was accomplished with the Darvan No. 2 as the dispersant.

Experiment 136 shows the two step procedure used to arrive at the maximum carbon loading.

With the Darco KB carbon, bentonite was selected as the thixotrope and Darvan No. 2 as the dispersant. To determine the optimum percent concentration of dispersant, a series of experiments were made and the results shown in Table XVII and Figure 4. Unlike the coal based carbon (CWS) suspensions, Darco KB wood based carbon slurries show a sharp drop in viscosity as the percent dispersant is raised to 5%. As shown in Figure 4, the viscosity of the 26% carbon loaded slurry was stabilized between 3% and 5% with only a slight decrease in viscosity at the 5% level.

The data indicates the optimum to be 3% of Darvan No. 2 dispersant with the carbon loading of 25.2%.

Table XVIII gives results of investigating sodium chromate and sodium silicate as the corrosion inhibitor. Although the suspension containing sodium silicate remained very stable during storage, the pH was unacceptably low at 6.1. Sodium chromate was selected as the corrosion inhibitor.

In finalizing the selection of the Darco KB carbon suspension, Experiments 159, 189 and 199, shown in Table XIX, were conducted. After 90 minutes mixing time, the suspensions showed large increases in viscosity with some friction heating being experienced with Experiment No. 199. Again solvent evaporation was not the apparent cause of the viscosity increase. Therefore, it is concluded that a thirty (30) minute mix time produces a uniform suspension with no improvements in stability by additional mixing.

Pigment evaluation shown by Experiments 159, 206, 207, and 208 in Table XX for the most part produced the same results as with the CWS carbon. Mapico 1100 yellow, iron oxide, gave a suitable olive green at 5.05% while higher concentrations (5.44%) of the cadmium lithopones resulted in color gradients ranging from dark green to black. Again the iron oxide pigment was chosen to give the olive green.

Of the different based carbons formulated and tested, the Darco KB appears to be the least attractive for a spray application. In order to prepare a sprayable slurry it was necessary to adjust the solvent content upward to 67.26% which gave a carbon content of 24.29%. The resulting viscosity measured 24 hours after mixing was 17,000 centipoise. As is characteristic of this particular carbon, the viscosity continues to drop during storage however does appear to stabilize after 30 days.

After formulation adjustments to give a sprayable system a typical formulation used for both testing sprayability and adhesion would be as follows:

	Actual	Percent
Ingredient	Weight	Formula Wt.
Carbon: Darco KB	325 g	24.29
Thixotrope: Bentonite	6 g	.45
Dispersant: Darvan No. 2	36 g	2.69
Pigment: 1100 Yellow	65 g	4.86
Corrosion Inhibitor: Sodium	•	
Chromate	6 g	.45
Solvent: (60/40 Water-Methanol)		
Mixing Time: Thirty (30) minutes Laboratory Homogeni		L-1
Typical Viscosity at 24 hours		s Helipath
after mixing		s #4 0 10 RPM
	7,450 cp	s #4 @ 20 RPM
pH Value	10.4	
Carbon Particle Size	1-2 μ (av	g.)

## TABLE XIV

DARCO	KB CARBO	ON - THI	XOTROPE	EVALUAT	LON	<del></del>	
FORMULATION NO.	95	96	97	103	104	106	
COMPOSITION BY/WT.		٠	Ac	tual Wt.	•		
Carbon DARCO KB - Wood Based Carbon	300 g	300 g	300 g	300 g	300 g	300 g	
Thixotrope (1) Bentonite	6 9	6 g	6 g				
(2) RG-244				6 g			
(3) COK -84					6 g		
(4) Nylon-6						6 g	
Dispersant (1) DAXAD 11	12 g	12 g	12 g	12 g	12 g	12 g	
(2) Darvan No. 2				·			
(3) Marasperse CB	<del> </del>			 			
(4) Nopcosant K	<u> </u>						
Picment 1100 Yellow	60 g	60 g	60 g	60 g	60 g	60 g	
Corrosive Inhibitor (1) Na C O	6 g	· 6 g	6 g	6 g	6 a	6 g	
(2)							
Solvent, Water/Alcohol 60/40 By Vol.	756 ML	956 ML	856° ML	856 ML	856 ML	856 ML	
MIXING TECHNIQUE: Homogenizer, min.		30	30		30	30	

# CHARACTERISTICS

Viscosi	ty. C		·····					r <del></del> -	
Imed.	Helipath "C"		10,000	16,000		14,000	12,800	•	
After	#4 @ 10 RPM	'	8,500	14,700		12,500	11,800		
Mix.	#4 @ 20 RPM	r i	4,200	7,650	i.	6,300	6,050		
After	Helipath "C"	2	8,000	15,000		11,000	10,000		
24	#4 @ 10 RPM	<u> </u>	7,000	13,200		10,800	9,300		
Hours	#4 @ 20 RPM	ه ۱	3,700	7,000		5,500	4,075		
After 7	Helipath "C"	e -	7.450	13,000	a i.e	9,000	9,000		
	#4 @ 10 RPM	a o	6,300	11,700	e o	8,900	7,700		
Days	#4 @ 20 RPM	is	3,300	6,175		4,600	3,950		
After	Helipath "C"	1 3	7,000	13,000		9,000	8,200		
14	#4 0 10 RPM	5	6,200	11,800		8,800	7,625		
Days	#4 @ 20 RPM	8	3,200	6,300	8	4,650	3,925		
	Helipath "C"	1	8,000	14,800	i	11,000	8,500		
After 30	#4 @ 10 RPM		6,800	13,550		10,350	7,625		
Days	#4 @ 20 RPM		3,625	7,200		5,350	4,000		
рН			8.8	8.8		8.3	7.7		

. MUTES:

DARCO	KB CARBO	ON - DIS	PERSANT	EVALUATION	<u> </u>	
FORMULATION NO.	97	112	113	105	148	
COMPOSITION BY/WT.	:		A	ctual Wt.		
Carbon DARCO KB - Wood Based Carbon	300 g	300 g	300 g	300 g	300 g	
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g	6 g	
(2)						- ties
(3)						
(4)					(Anmonyx 85	6)*
Dispersant (1) DAXAD 11	12 g				12 g	
(2) Nopcosant K	ļ	12 g				
(3) Marasperse CB	<b></b>		12 g			
(4) Darvan No. 2	<u> </u>			12 g		
Pigment 1100 Yellow	60 g	60 g	60 g	60 g	60 g	
Corrosive Inhibitor (1) Na C O	6 g	6 g	6 g	6 9	6 g	
(2)						
Solvent, Water/Alcohol 60/40 By Vol.	856 ML	856 ML	856 ML	856 ML	856 ML	
MIXING TECHNIQUE: Homogenizer, min.	30	30	30	30	30	,

	_				
CHA	~ *	^-		7 ~ 7	. 4 ~ ~
IMA	- L				
LIL			LR	1 -3 I	

V1s cost	ity. C)						
Imed.	Helipath "C"	16,000	30,000	13,000	7,000	41,000	<u> </u>
After	#4 @ 10 RPM	14,700	26,000	11,540	6,700	12,300	
Mix	#4 @ 20 RPM	7,650	13,950	6,000	3,475	12,100	
After	Helipath "C"	15,000	19,000	11,000	4,200	32,000	
24	#4 @ 10 RPM	13,200	18,800	9,400	3,800	12,000	
Hours	#4 @ 20 RPM	7,000	9,850	4,950	2,075	11,400	
After	Helipath "C"	13,000	18,200	7,300	4,000	28,000	
7	#4 @ 10 RPM	11,700	16,000	6,300	3,100	12,000	
Days	#4 @ 20 RPM	6,175	8,425	3,350	1,700	11,750	
After	Helipath "C"	13,000	15,000	6,000	3,800	30,000	
14	#4 @ 10 RPM	11,800	14,600	4,900	3,200	13,000	1
Days	#4 @ 20 RPM	6,300	7,700	2,600	1,700	12,650	
• • •	Helipath "C"	14,800	16,000	6,900	4,000	30,000	
After 30	#4 @ 10 RPM	13,550	15,500	5,600	3,600	13,800	
Days	#4 @ 20 RPM	7,200	8,150	2,950	1,950	12,600	
рН		8.8	8.3	7.9	7.8	7.6	

TABLE XVI

PARAMI ATTAN AND			1	1		1
FORMULATION NO.	133	136	143	142	 	-
COMPOSITION BY/WT.			Ac	tual Wt.		
Carbon DARCO KB - Wood Based Carbon	300 g	325 g	325 g	325 g		
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g		
. (2)						
(3)						
(4)						
Dispersant (1) DAXAD 11	24 g					
(2) Darvan No. 2		12 + 12	24 g			
(3) Marasperse CB				24 9	 	
(4)	+				 	
Pigment 1100 Yellow	60 g	60 g	60 g	60 g	 	
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>0</sub>	6 g	6 g	6 g	6 g	 	
(2)						
Solvent, Water/Alcohol 60/40 By Vol.	856 ML	856 ML	856 ML	856 ML		
MIXING TECHNIQUE: Homogenizer, min.	30	30 + 3	30	30		

CM	A D A	~	CD.	I C T	100
UTV	100		ER.	131	I CS

Vis cost	ty, CP	· ·	(33,000	)	·	 		
Imed.	Helipath "C"	32,000	25,000	25,000	42,000	<u> </u>	٠	<u> </u>
After	#4 0 10 RPM	31,400	24,000	22,700	34,000			
Mix.	#4 @ 20 RPM	16,500	12,300	12,200	19,250			
After	Helipath "C"	32,000	21,000	21,000	35,000			A TOUR
24	#4 0 10 RPM	31,300	20,800	20,800	30,000			
Hours	#4 @ 20 RPM	16,450	10,500	11,000	17,250			
After	Helipath "C"	32,000	20,500	19,000	24,500			
7	#4 @ 10 RPM	30,600	20,100	18,800	23,600			
Days	#4 @ 20 RPM	16,050	10,300	9,950	12,400			
After	Helipath "C"	34,000	22,000	20,000	24,500			
14	#4 @ 10 RPM	33,000	23,600	19,600	24,200			
Days	#4 -0 20 RPM	17,550	12,000	10,350	12,650			
4.64	Helipath "C"	34,500	25,000	23,000	31,000			
After 30	#4 @ 10 RPM	32,200	26,600	22,600	30,200			
Days	#4 @ 20 RPM	17,100	13,700	11,900	15,900			
рН		7.7	8.0	7.9	7.9			7 t m.

MULES

TABLE XVII

DARCO KB CA	DARCO KB CARBON - % DISPERSANT EVALUATION								
FORMULATION NO.	148	155	156	158	162		-		
COMPOSITION BY/WT.			Ac	tual Wt.	•				
Carbon DARCO KB - Wood Based Carbon	300 g	300 g	300 g	300 g	300 g				
Thixotrope (1) Bentonite	6 q	6 q	6 q	6 g	6 g				
(2)							1		
(3)									
(4)									
Dispersant (1) Darvan No. 2	12 g	24 g	36 g	48 g	60 g				
(2)									
(3)	·								
(4)									
Pigment 1100 Yellow	60 g	60 g	60 g	60 g	60 a				
Corrosive Inhibitor (1) NagC_O,	6 g	6 g	6 g	6 g	6 g				

856 ML

30

## CHARACTERISTICS

(2)
Solvent, Water/Alcohol 60/40 By Vol.

MIXING TECHNIQUE: Homogenizer, min.

V1s cos 1	Viscosity, CP									
Imed.	Helipath "C"	7,000	13,500	10,000	9,000	1,000				
After	#4 @ 10 RPM	6,700	13,300	8,800	5,100	525				
Mix	#4 @ 20 RPM	3,475	6,800	4,500	2,625	350				
After	Helipath "C"	4,200	10,500	7,000	5,500	500				
24	#4 @ 10 RPM	3,800	10,800	6,500	3,300	300				
Hours	#4 @ 20 RPM	2,075	5,600	3,350	1,750	250				
After	Helipath "C"									
7	#4 @ 10 RPM									
Days	#4 @ 20 RPM									
After	Helipath "C"									
14	#4 0 10 RPM									
Days	#4 @ 20 RPM									
164	Helipath "C"	· ·								
After 30	#4 @ 10 RPM									
Days	#4 6 20 RPM									
рH									Bavas	

856 ML 856 ML

30

30

856 ML

- 30

856 ML

30

MUTES:

## TABLE XVII (Cont'd)

	DARCO KB C	ARBON - 9	DISPER	SANT EV	ALUATION			
FORMULATION NO.		157	143	159	160	163		
COMPOSITION BY/WT.	·			A	' ctual Wt	•		
Carbon DARCO KB	- Wood Based Carbon	325 g	325 g	325 g	325 g	325 g		
Thixotrope	(1) Bentonite	6 g	6 g	6 g	6 g	6 g		
	(2)							
	(3)							
	(4)							
Dispersant	(1) Darvan No. 2	12 g	24 g	36 g	48 g	60 g		
***	(2)							
	(3) (4)	-						
Pigment	ll00 Yellow	60 g	60 g	60 g	60 g	60 g		
Corrosive I	nhibitor (1) Na_C_O,	6 g	6 g	6 g	6 g	6 g		
	(2)							
Solvent, Water/Al	cohol 60/40 By Vol.	856 ML	856 ML	856 ML	856 ML	856 ML		
MIXING TECHNIQUE	Homogenizer, min.	30	30	30	30	30		
CHARACTERISTICS								
V1s cos 1	ty, CP							
Imed.	Helipath "C"	29,000	25,000	14,000	13,500	13,000	·	
After	#4 @ 10 RPM	24 800	22 700	11.900	10.400	7.450		

V1s cos	ty, C							
Imed.	Helipath "C"	29,000	25,000	14,000	13,500	13,000	,	
After	#4 @ 10 RPM	24,800	22,700	11,900	10,400	7,450		
Mix	#4 @ 20 RPM	14,800	12,200	5,925	5,325	3,925		
After	Helipath "C"	22,000	21,000	10,000	9,000	7,500		
24	#4 @ 10 RPM	21,500	20,000	8,900	6,800	4,450		
Hours	#4 @ 20 RPM	11,950	11,000	4,550	3,575	2,500		
After	Helipath "C"							
7	#4 @ 10 RPM							
Days	#4 0 20 RPM							
After	Helipath "C"		•					
14	#4 @ 10 RPM							
Days	#4 @ 20 RPM							
Afaan	Helipath "C"							
After 30	#4 @ 10 RPM							
Days	#4 0 20 RPM							
pH							 12.72	Maria Distanti

خلاله

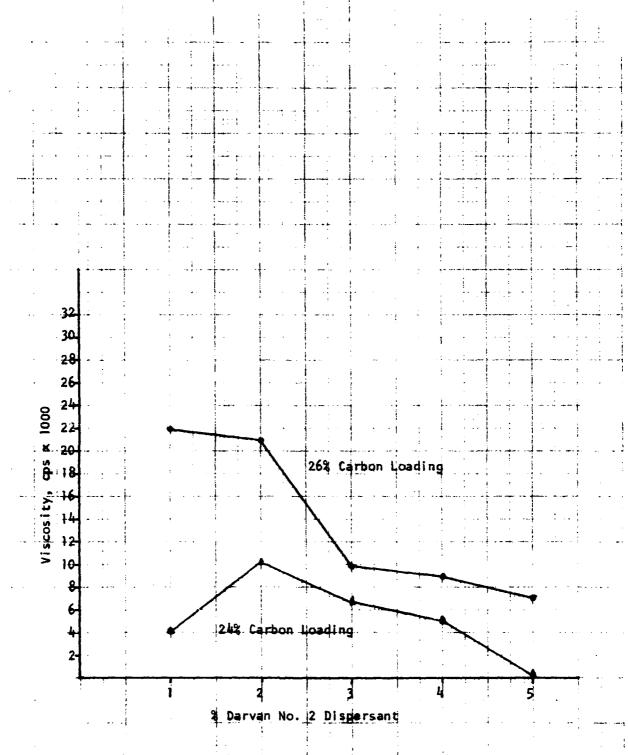


FIGURE 4 - EFFECT OF & DISPERSANT ON DARCO HB CARBON SLURRIES

# TABLE XVIII

DAR	CO KB - CORROSI	ON INHIE	BITOR EV	ALUATION	 · · · · · · ·	, !
FORMULATION NO.	101	102	108		 	
COMPOSITION BY/WT.		·	Ac	ctual Wt.		
Carbon DARCO KB - Wood Based Ca	rbon 300 g	300 g	300 g			
<u>Ihixotrope (1) Bentonite</u>	12 g	12 g	12 g			
(2)		,				
(3)						
(4)						
Dispersant (1) DAXAD 11	12 g	12 g	12 g			
(2)						
(3)				·		
(4)						
Pigment 1100 Yellow	60 g	60 g	60 g			
Corrosive Inhibitor (1) Na	C 0, 6 g		12 g			
(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>		6 g				
Solvent, Water/Alcohol 60/40 By V	01. 856 ML	856 ML	856 ML			
MIXING TECHNIQUE: Homogenizer, m	in. 30	30	30			

## CHARACTERISTICS

V1s cos	ity, CP			
Imed.	Helipath "C"	21,000 16,00	16,000	<u> </u>
After	#4 0 10 RPM	19,200 14,50	14,350	
Mix	#4 @ 20 RPM	9,600 7,67	7,400	
After	Helipath "C"	21,000 16,00	14,000	
24	#4 @ 10 RPM	18,400 13,90		
Hours	#4 @ 20 RPM	9,200 7,45	6,800	
After	Helipath "C"	19,000 16,00	15,000	
7	#4 @ 10 RPM	16,200 13,82	13,750	
Days	#4 @ 20 RPM	8,750 7,42	7,150	
After	Helipath "C"	19,800 16,00	15,000	
14	#4 @ 10 RPM	17,050 14,20	13,640	
Days	#4 @ 20 RPM	9,200 7,65	7,075	
• • •	Helipath "C"	22,000 16,00	14,000	
After 30	#4 @ 10 RPM	19,100 15,00	13,200	
Days	#4 @ 20 RPM	11,400 7,95	6,500	
pH		8.8 6.1	8.0	

MUTES:

DARCO K	3 - MIXI	NG TIME	EVALUAT	ION		 , -
FORMULATION NO.	159	189	199			 _
COMPOSITION BY/WT.			Ac	tual Wt.		
Carbon Darco KB - Wood Based Carbon	325 g	<b>3</b> 25 g	325 g	325 g	325 g	<u></u>
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g	6 g	<u> </u>
(2)			<u>·</u>			-
(3)						
(4)						
Dispersant (1) Darvan No. 2	36 g	36 g	36 g	36 g	36 g	 
(2)		_				1
(3)						
(4)						
Pigment 1100 Yellow	60 g	60 g	60 g	60 g	60 g	<del>                                     </del>
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 9	6 g	6 g	 
(2)						
Solvent, Water/Alcohol 60/40 By Vol. ml	856	856	856	856	856	 
MIXING TECHNIQUE: Homogenizer, Minutes	30	60	90	120	180	<u> </u>

Viscosi	ity, CP		
Imed.	Helipath "C"	14,000 55,000 94,000	
After	#4 @ 10 RPM	11,900 30,000 45,000	
Mix	#4 @ 20 RPM	5,925 22,000 33,000	
After	Helipath "C"	10,000 42,000	
24	#4 @ 10 RPM	8,900 27,000	
Hours	#4 0 20 RPM	4,550 19,500	
After	Helipath "C"	8,500 42,000	
7	#4 @ 10 RPM	7,900 36,000	
Days	#4 @ 20 RPM	4,250 19,600	
After	Helipath "C"	8,000 43,000	
14	#4 @ 10 RPM	7,400 37,000	
Days	#4 @ 20 RPM	3,825 18,500	
	Helipath "C"	8,500 44,000	
After 30	#4 @ 10 RPM	8,000 28,500	
Days	#4 @ 20 RPM	4,175 20,500	
Tu .			
Solv	vent Content, %	59.4 58.4 -50-	

TABLE XX

	DARCO K	B - PIG	MENT EVA	LUATION	1		
FORMULATION NO.		159	206	207	208		
COMPOSITION BY/WT.				A	ctual Wt.		
Carbon Darco KB		325 g	325 g	325 g	325 g		
Thixotrope (1) Be	ntonite	6 g	6 g	6 g	6 g		
(2)							
(3)	·						
(4)							
Pigment (1) 110	00 Yellow	60 g	65 g				
(2) Az	o Yellow			65 g			
(3) Ca	d Yellow/Cad Orang	e			56/5 g		
(4)							
Dispersant: Da	rvan No. 2	36 g	36 g	36 g	36 g		
Corrosive Inhibite	or (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 g	6 g		
(2)							
Solvent, Water/Alcohol (	50/40 By Vol., ml	756	756	756	756		
MIXING TECHNIQUE: Homog	enizer, minutes	30	30	30	30	}	<b>1</b>

V1s cos 1	ity, CP				···	<b></b>		<del></del>	<b></b>	<sub>r</sub> <b></b>
Imed.	Helipath "C"		14,000	32,000	76,000	15,000				
After	#4 9 10 RPM		11,900	27,000	After	13,500				
Mix	#4 @ 20 RPM		5,925	14,300	2 min.	16,500				
After	Helipath "C"		10,000	24,000						
24	#4 @ 10 RPM		8,900	23,700						
Hours	#4 @ 20 RPM		4,550	11,850						
	-	Color,	Olive	01ive		Dark				
		Wet	Green	Green	Black	Green				
	•	Color.	Olive	Olive		Dark				
		Dry	Green	Green	Black	Green	<del></del>			-
	1									
<b>*</b>										
ρН										

MUTES:

#### (3) ACC Carbon - Petroleum Coke Based

The petroleum based carbon was supplied by Union Carbide in granular form. The pH value in aqueous solution measured 10.4. The surface area is 980-1080 square meters/gram with a CCL<sub>A</sub> activity of 63%.

As discussed in the materials section of this report, a 25 pound batch of ACC carbon was ball milled for 48 hours. The average particle size after milling was 0.7  $\mu$  as determined by the Sub-Sieve Analyzer. Although this particle size is slightly less than desired (1-2  $\mu$ ), slurries were prepared for testing the thixotropic and dispersing agents. An additional 25 pound batch of ACC was prepared to the desired 1-2  $\mu$  concurrently with the experiments and was used to establish final selection of ingredients.

Experiments 98, 99, 122, 123, 124, and 125 as shown in Table XXI were prepared to test the efficiency of the bentonite, asbestos, pyrogenic silica and microcrystalline nylon as thixotropes. As the results show, bentonite was the most efficient thixotrope by giving the highest viscosities. The data also shows the effect of particle sizes on both the viscosity and stability during storage. By comparing experiments 99 and 122 it can be seen that slurries prepared with ACC carbon with an average particle size of 1.4  $\mu$  remains more stable during storage than those prepared with 0.7  $\mu$  carbon particles.

After selecting bentonite as the best thixotrope with ACC carbon, slurries were prepared to evaluate each of the dispersants. Results are shown in Table XXII with carbon loadings of 36.3%. Experiment 127 using Marasperse CB gave the lowest viscosity with ACC petroleum based carbon and was used in further evaluation.

It should be noted that results reported in Table XXII were obtained using ACC carbon with an average particle size of 0.7  $\mu_{\text{\tiny J}}$  all of which show unacceptable stability. This series of experiments to select the most efficient dispersant was re-run using ACC carbon with a particle size of 1-2  $\mu_{\text{\tiny L}}$ 

To prepare the desired particle size, a 25 pound batch of ACC carbon was pulverized using the Mikro-Pulverizer and then ball milled for 4-1/2 hours. The average particle size after milling was 1.10  $\mu$  as determined by the Sub-Sieve Analyzer.

Using Bentonite as the thixotrope, slurries were prepared to evaluate the various dispersants with the ACC carbons. As shown in Table XXII, Nopcosant K dispersant produces an unmixable slurry, thus was eliminated from further consideration. Experiments 167, 168, and 169, shown in Table XXIII, were conducted to investigate the most efficient dispersant. Although Marasperse CB gave the lowest viscosity, Experiment 167, with a carbon loading of 36.3%, attempts to raise the viscosity by additional carbon were unsuccessful. Carbon loadings over 36.3% result in the formation of heavy glue-like texture that would be impractical to spray. Dispersants DAXAD 11 and Marasperse CB produced slurries that form the gel-like suspension after 24 hour storage.

By comparing Experiments 167 and 169, it can be seen that DAXAD II dispersant produces a slurry that increases in viscosity during storage, whereas the Darvan No. 2 slurry will decrease during storage. Since a decrease in viscosity during storage is more desirable for a spray application than is an increase, the Darvan No. 2 was selected as the optimum dispersant.

After selecting the Darvan No. 2 dispersing agent for use with the ACC carbon, Experiments 180, 181, 182, 183, and 186 were conducted to determine the optimum percent. As shown in Table XXIV, slurries containing 2, 3, and 4 percent of Darvan No. 2 gave no significant decreases in viscosity, however in order to produce a thixotrope capable of holding 36% carbon in suspension, it was necessary to increase the thixotrope (bentonite) content from .45% to .67%. These results are also charted in Figure 5.

Table XXV show results of evaluating sodium chromate and sodium silicate as corrosion inhibitors in the ACC carbon slurries. Although the sodium chromate resulted in a higher pH, the sodium silicate suspension gave a higher degree of stability during storage. A preliminary selection of sodium chromate was made based on the higher pH, however additional storage data proved sodium silicate to be the superior corrosion inhibitor.

The effect of additional mixing times was next evaluated on the ACC suspensions. As shown in Table XXVI, additional mixing produced the least changes in viscosity of the four different based carbons evaluated. After three (3) hours the increase was only 6,000 centipoise with approximately 4% of the solvent being lost due to evaporation. Here again the gel-like structure was formed after 24 hours storage with the thirty (30) minute mixing time. Unlike any of the other carbon suspensions tested, mixing time with the ACC suspension can be used to produce a viscosity desirable for spraying.

ACC carbon slurries containing sodium silicate as the corrosion inhibitor show a very high degree of stability. As can be seen by Table XXVII, ACC suspensions prepared with sodium silicate do not change in viscosity after static storage for 30 days and longer. Similar suspensions prepared with sodium chromate show a sharp drop in viscosity during a 30 day storage time. Although the pH is slightly lower in suspensions containing sodium silicate,  $(\sim 8.0)$  it is felt that the high degree of stability is the more important property.

Based on the results discussed above, using the ACC carbon, the following selection can be made.

Ingredient	Actual Weight	
Carbon: ACC	470 g	34.99
Thixotrope: Bentonite	9 (	.67
ispersant: Darvan No. 2	24	1.79
Pigment: 1100 yellow	78 g	5.81
Corrosion Inhibitor: Sodium	_	
Silicate	6 9	.45
Solvent: (60/40 Water-Methanol)	756 n	nl 55.29
Mixing Time: Thirty (30) minutes Laboratory Homogeniz		the L-1
Typical Viscosity at 24 hours		cps Helipath
after mixing	4,000	) cps #4 @ 10 RPM
•	2,300	) cps #4 @ 20 RPM
pH Value	8.0	•
Carbon Particle Size	1.1 1	(avg.)

AC	C CARBON	- THIX	TROPE E	ALUATIO	<b>L</b>	<del></del>	<del></del>
FORMULATION NO.	98	99	122	123	124	125	
COMPOSITION BY/WT.			Ac	tual Wt.	•		
Carbon ACC - Petroleum Coke Based		480 <sup>2</sup> g	480 <sup>3</sup> g	480 <sup>3</sup> g	480 <sup>3</sup> g	480 <sup>3</sup> g	
Thixotrope (1) Bentonite	6 g	6 g	6 g				
(2) RG-244				6 g			
(3) cok-84					6 g		
(4) Nylon-6 (Powder)						6 9	
Dispersant (1) DAXAD 11	12 g	12 g	12 g	12 g	12 g	12 g	
(2) Darvan No. 2							
(3) Marasperse CB	<del> </del>						<b></b>
(4) Nopcosant K	<b></b>						
Pignent 1100 Yellow	60 g	60 g	60 g	60 g	60 g	60 g	
Corrosive Inhibitor (1) Na C O.	6 g	6 g	6 g	6 g	6 g	6 9	
(2)							
Solvent, Water/Alcohol 60/40 By Vol.	756 ML	756 ML	756 ML	756 ML	756 ML	756 ML	
MIXING TECHNIQUE: Homogenizer, min.	30	30	30	30	30	30	

Viscos1	ity. O		,	<del></del>			·	<del></del>	
Imed.	Helipath "C"	7,000	13,000	13,000	8,000	6,000	4,000		
After	#4 @ 10 RPM	5.500	11,700	8,500	4,500	4,000	2,200		<del></del>
Mix.	#4 @ 20 RPM	2,800	6,100	4,650	2,450	2,150	1,250		
After	Helipath "C"	6,000	12,500	25,000	19,000	11,000	9,000		
24	#4 @ 10 RPM	5,300	11,000	18,000	16,100	6,700	6,700		
Hours	#4 @ 20 RPM	2,750	5,825	9,150	7,950	3,450	3,250		
After	Helisath "C"	6,700	12,500	23,000	19,000	10,000	8,000		
7	#4 @ 10 RPM	5,300	11,200	17,200	16,000	6,775	5,300		
Days	#4 0 20 RPM	2,775	5,900	8,700	7,950	3,350	2,700		
After	Helipath "C"	7,000	13,000	27,000	19,000	10,000	9,000		
14	#4 0 10 RPM	5,500	10,500	19,400	14,850	7,100	6,200		
Days	#4 @ 20 RPM	2,850	5,600	10,100	7,600	3,550	3,200		
	Helipath "C"	7,000	12,000	34,000	30,000	16,000	13,500		
After 30	#4 0 10 RPM	5,700	10,400	27,200	23,200	9,300	10,450		
Days	#4 @ 20 RPM	2,900	5,650	14,000	12,400	4,625	5,150		
рH		11.0	10.8	9.2	9.2	9.3	9.2		

<sup>1.</sup> Bal: milled 24 hours - Particle Size Average 1.65  $\mu$  in 1-2 lb. batch size 2. Ball milled 48 hours - Particle Size Average 1.40  $\mu$  in 1-2 lb. batch size ... Ball milled 24 hours - Particle Size Average 0.70  $\mu$  in 25 lb. batch size

AC	C CARBON	S - DIS	PERSANT	EVALUATI	ON	<del></del>	
FORMULATION NO.	122	126	127	127-A	128	-	
COMPOSITION BY/WT.			. A	ctual Wt.	•		
Carbon ACC - Petroleum Coke Based	480 g	480 g	480 g	528 g	480 g		
Inixotrope (1) Bentonite	6 g	6 g	6 g	12 g	6 g		
(2)					<u> </u>		
. (3)							
(4)							÷
Dispersant (1) DAXAD 11	12 g						
(2) Darvan No. 2		12 g					
(3) Marasperse CB	<b></b>		12 g	12 g			
(4) Nopcosant K					12 g		
Pignent 1100 Yellow	60 g	60 g	60 g	60 g	60 g		
Corrosive Inhibitor (1) NagC 0.	6 g	6.9	6 g	6 g	6 g		
(2)							
Solvent, Water/Alcohol 60/40 By Vol.	756 ML	756 ML	756 ML	'756 ML	756 ML		
MIXING TECHNIQUE: Homogenizer, min.	30	30	30	30	30		v

CHA	DΔ	ГΤ	CDI		T 7	rc
CHA		u	CK1	3	1	w

Viscosi	ity, CP						 	
Imad.	Helipath "C"	13,000	34,000	2,000	38,000	<u> </u>	<u> </u>	ļ
After	#4 @ 10 RPM	8,500	28,800	900	19,000	<u> </u>		
Mix.	#4 @ 20 RPM	4,650	15,300	575	10,350	I'		
After	Helipath "C"	25,000	22,000	1,000	17,000			
24	#4 @ 10 RPM	18,000	18,350	500	7,950			
Hours	#4 @ 20 RPM	9,150	9,600	325	4,700			
After	Helipath "C"	23,000	14,000	500	7,000	1 X		
7	#4 # 10 RPM	17,200	10,850	250	3,700	de o		
Days	#4 9 20 RPM	8,700	5,700	175	2,300	S	1	
After	Helipath "C"	27,000	12,000	400	6;000			
14	#4 9 10 RPM	19,400	9,950	200	2,900	- × ×		
Days	#4 @ 20 RPM	10,100	5,150	175	1,800	8		
4.64	Helipath "C"	34,000	14,500	500	7,000			
After 30	#4 @ 10 RPM	27,200	12,000	300	3,700			
Days	#4 0 20 RPM	14,000	6,150	225	2,250			
pH		9.2	9.3	9.2	9.3			
FORM	ULATION MADE W	√ITH .7 µ CARBON	-56-				 -	<u> </u>

FORMULATION NO.	167	168	169					<b></b>
COMPOSITION BY/WT.			A	' ctual Wt	•			
Carbon ACC Petroleum Coke Based	480 g	480 g	480 g					
Thixotrope (1) Bentonite	6 9	6 g	6 g					
								· 'VE;
(3)								
. (4)								
Dispersant (1) Darvan No. 2	12 g							
(2) Marasperse CB		12 g						
(3) DAXAD 11		<b>}</b>	12 g			<del></del>	<del>                                     </del>	
(4) Nopcosant K	_	Elimina	ted - (	ef. For	ulation	128)		
Piument 1100 Yellow	60 g	60 g	60 q					
Corrosive Inhibitor (1) Na2Cr04	6 g	6 g	6 g					
_(2)								
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756					
MIXING TECHNIQUE: Homogenizer, minutes	30	30	30				1	

V1s cos	ity, CP				<u> </u>	 		
Imed.	Helipath "C"	13,000	1,500	10,000			<u> </u>	
After	#4 @ 10 RPM	8,000	700	7,400				
Mix	#4 0 20 RPM	4,350	475	4,000				
After	Helipath "C"	9,000	1,000	12,000				2.23.1.00
24	#4 @ 10 RPM	5,600	500	10,450				
Hours	#4 @ 20 RPM ·	3,100	.350	5,450				
After	. Helipath "C"	4,900	400	13,500				
7	#4 @ 10 RPM	2,950	300	10,300				
Days	#4 0 20 RPM	1,750	225	5,350	•			
After	Helipath "C"	4,000	300	15,000				
14	#4 @ 10 RPM	2,450	250	11,500				
Days	#4 @ 20 RPM	1,500	200	5,900				
	Helipath "C"	6,000		15,000				
After 30	#4 @ 10 RPM	2,850	.30	14,600			1	
Days	#4 @ 20 RPM	1,700	50.00	7,400			1	
рН		9.1	9.3	9.2				

 $\frac{\text{hullS:}}{\text{-57-}}$  Formulations prepared with 1.10  $\mu$  carbon.

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# TABLE MXIV

ACC C	ARBON -	PERCENT	DISPERS	ANT EVALUATI	ON	
FORMULATION NO.	180	181	182	183	186	
COMPOSITION BY/WT.			Ac	tual Wt.		
Carbon ACC - Petroleum Coke Based	480 g	480 g	480 g	480 g	480 g	
Thixotrope (1) Bentonite	6 g	6 g	6 9	6 g	9 9	
(2)						
(4)		- 4				
Dispersant (1) Dervan No. 2 (2)	12 g	24 g	36 g	48 g	24 g	
Pigment 1100 Yellew	60 g	60 g	60 g	60 g	60 g	
Corrosive Inhibitor (1) Na2Cr04	6 g	6 g	6 g	6 g	6 g	
(2)						
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756	756	756	
MIXING TECHNIQUE: Homogenizer, minutes	30	30	30	30	30	

#### CHARACTERISTICS

Viscosi	ity. CP					_ · · <del> </del>	
Imed.	Helipath "C"	14,000	1,800	1,500	2,000	9,000	
After	#4 #.10 RPM	8,150	900	900	1,225	5,250	
Mix	#4 @ 20 RPM	4,650	650	625	825	3,225	
After	Helipath "C"	7,200	700	800	1,000	4,000	
24	#4 @ 10 RPM ·	4,400	500	500	625	2,300	
Hours	#4 @ 20 RPM	2,650	375	375	475	1,500	
After	Helipath "C"						
7	#4 @ 10 RPM						
Days	#4 @ 20 RPM						
After	Helipath "C"						
14	#4 @ 10 RPM						<u> </u>
Days	#4 @ 20 RPM						
	Helipath "C"						
After 30	#4 @ 10 RPM						•
Days	#4 @ 20 RPM						
рН						•	

Formulations prepared with 1.10  $\mu$  carbon. -58-

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## TABLE XXV

ACC CA	RBON -	ORROSION	I INHIBITOR EVALUATION	
FORMULATION NO.	186	187		
COMPOSITION BY/WT.			Actual Wt.	
Carbon ACC - Petroleum Coke Based	480 g	480 g		
Thixotrope (1) Bentonite	9 9	9 9		
(2)				
(3)				
(4)				
Dispersant (1) Darvan No. 2	24 g	24 g		
(2)				
(3)				
(4)				
Pigment 1100 Yellow	60 g	60 g		
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g			
(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>		6 g		
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756		
MIXING TECHNIQUE: Homogenizer, minutes	30	30		

CHA	ΛG	CT	בט	TC	T 3	CC
L.HA	KA	LI	rк	1.5	11	$r_2$

ity, CP								
Helipath "C"	9,000	6,000				1	[	
#4 @ 10 RPM	5,250	3,900						_
#4 @ 20 RPM	3,225	2,400						
Helipath "C"	4,000	5.500					200.00	*
#4 @ 10 RPM	بمستملت فتتناقب						<b>†</b>	
#4 @ 20 RPM	1,500	2,300						-
Helipath "C"	1,500	6,000						
#4 @ 10 RPM	1,100	4,500						_[
#4 @ 20 RPM	850	2,750						
Helipath "C"	1,000	6,000						-
#4 @ 10 RPM	85C	4,400						
#4 @ 20 RPM	700	2,725			1			•
Helipath "C"	1,000	6,000						_
#4 @ 10 RPM	800	4,500						_
#4 @ 20 RPM	700	2,800		1		<b>†</b>	<del> </del>	-
<u> </u>	8.9	8.0					-	-
	Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM	Helipath "C"       9,000         #4 @ 10 RPM       5,250         #4 @ 20 RPM       3,225         Helipath "C"       4,000         #4 @ 10 RPM       2,300         #4 @ 20 RPM       1,500         Helipath "C"       1,500         #4 @ 10 RPM       850         Helipath "C"       1,000         #4 @ 10 RPM       85C         #4 @ 20 RPM       700         Helipath "C"       1,000         #4 @ 10 RPM       800         #4 @ 10 RPM       800         #4 @ 20 RPM       700	Helipath "C"       9,000 6,000         #4 @ 10 RPM       5,250 3,900         #4 @ 20 RPM       3,225 2,400         Helipath "C"       4,000 5,500         #4 @ 10 RPM       2,300 3,650         #4 @ 20 RPM       1,500 6,000         #4 @ 10 RPM       1,100 4,500         #4 @ 20 RPM       850 2,750         Helipath "C"       1,000 6,000         #4 @ 10 RPM       85C 4,400         #4 @ 20 RPM       700 2,725         Helipath "C"       1,000 6,000         #4 @ 10 RPM       800 4,500         #4 @ 10 RPM       800 4,500         #4 @ 20 RPM       700 2,800	Helipath "C"       9,000       6,000         #4 @ 10 RPM       5,250       3,900         #4 @ 20 RPM       3,225       2,400         Helipath "C"       4,000       5,500         #4 @ 10 RPM       2,300       3,650         #4 @ 20 RPM       1,500       2,300         Helipath "C"       1,500       6,000         #4 @ 10 RPM       850       2,750         Helipath "C"       1,000       6,000         #4 @ 10 RPM       850       4,400         #4 @ 10 RPM       700       2,725         Helipath "C"       1,000       6,000         #4 @ 10 RPM       800       4,500         #4 @ 10 RPM       800       4,500         #4 @ 20 RPM       700       2,800	Helipath "C"       9,000       6,000         #4 @ 10 RPM       5,250       3,900         #4 @ 20 RPM       3,225       2,400         Helipath "C"       4,000       5,500         #4 @ 10 RPM       2,300       3,650         #4 @ 20 RPM       1,500       2,300         Helipath "C"       1,500       6,000         #4 @ 10 RPM       850       2,750         Helipath "C"       1,000       6,000         #4 @ 10 RPM       85c       4,400         #4 @ 20 RPM       700       2,725         Helipath "C"       1,000       6,000         #4 @ 10 RPM       800       4,500         #4 @ 10 RPM       800       4,500         #4 @ 20 RPM       700       2,800	Helipath "C" 9,000 6,000  #4 @ 10 RPM 5,250 3,900  #4 @ 20 RPM 3,225 2,400  Helipath "C" 4,000 5,500  #4 @ 10 RPM 2,300 3,650  #4 @ 20 RPM 1,500 2,300  Helipath "C" 1,500 6,000  #4 @ 10 RPM 850 2,750  Helipath "C" 1,000 6,000  #4 @ 10 RPM 850 4,400  #4 @ 20 RPM 700 2,725  Helipath "C" 1,000 6,000  #4 @ 20 RPM 800 4,500  #4 @ 10 RPM 800 4,500	Helipath "C" 9,000 6,000  #4 @ 10 RPM 5,250 3,900  #4 @ 20 RPM 3,225 2,400  Helipath "C" 4,000 5,500  #4 @ 10 RPM 2,300 3,650  #4 @ 20 RPM 1,500 2,300  Helipath "C" 1,500 6,000  #4 @ 10 RPM 850 2,750  Helipath "C" 1,000 6,000  #4 @ 10 RPM 85C 4,400  #4 @ 20 RPM 85C 4,400  #4 @ 20 RPM 700 2,725  Helipath "C" 1,000 6,000  #4 @ 10 RPM 800 4,500  #4 @ 10 RPM 800 4,500	Helipath "C" 9,000 6,000 9 9,0

Mile: Particle Size 1.10 µ

N - MIX	ING TIME	EVALUAT	TION			-, -
186	190	198	200	202		
·		Ac	tual Wt.			
480 g	480 g	480 g	480 g	480 g		
9 9	9 g	9 9	9 g	9 g		
						VE.
	<u> </u>					
24 g	24 g	24 g	24 g	24 g		
(0		(0)	(0 =	60 =		
60 g	60 g	60 g	60 g			<b></b>
6 g	6 g	6 g	6 g	6 g		
756	756	756	756	756		
30	60	90	120	180		
	186 480 g 9 g 24 g 60 g 6 g	186 190  480 g 480 g  9 g 9 g  24 g 24 g  60 g 60 g  6 g 6 g	186 190 198  Ac  480 g 480 g 480 g  9 g 9 g 9 g  24 g 24 g 24 g  60 g 60 g 60 g  6 g 6 g 6 g  756 756 756	Actual Wt.  480 g 480 g 480 g 480 g  9 g 9 g 9 g 9 g  24 g 24 g 24 g 24 g  60 g 60 g 60 g 60 g  6 a 6 g 6 g 6 g  756 756 756 756 756	186 190 198 200 202  Actual Wt.  480 9 480 9 480 9 480 9 480 9  9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9 9	186 190 198 200 202  Actual Wt.  480 g 480 g 480 g 480 g 480 g  9 g 9 g 9 g 9 g 9 g  24 g 24 g 24 g 24 g 24 g  60 g 60 g 60 g 60 g 60 g  6 g 6 g 6 g 6 g 6 g  756 756 756 756 756 756

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Imed.	Helipath "C"	9,000	8,000	10,500	11,000	16,000		<u>.</u>	
After	#4 0 10 RPM	5,250	1	6,600	7,100	8,800			<u></u>
Mix	#4 0 20 RPM	3,225	3,200	4,000	4,350	5,300		J.	
After	Helipath "C"	4,000	4,500	7,000	6,000	10,000			
24	#4 @ 10 RPM	2,300	2,700	4,200	3,400	6,100			
Hours	#4 @ 20 RPM	1,500	1,800	2,700	2,300	3,900			
After	Helipath "C"	1,500	2.000	3,800	5.000	7,000			
7	#4 @ 10 RPM	1,100	1,500	2,350	[	4,150			
Days	#4 @ 20 RPM	850	1,100	1,700		2,775			
After	Helipath "C"	1,000	1,500	2,500	4,000	5,000			
14	#4 @ 10 RPM	850	1,100	1,900	2,800	3,500	L		
Days	#4 @ 20 RPM	700	900	1,450	2,075	2,550			
	Helipath "C"	1,000	1,500	3,000	6,000	6,000			
After 30	#4 @ 10 RPM	800	1,300	2,100	3,700	3,900			
Days	#4 @ 20 RPM	700	1,050	1,625	2,700	2,800			
рН		8.9	9.0	9.0	9.0	9.0			Aut : DAY
Solve	ent Content, %	55.7				51.8	1	<b></b>	- <del></del>

Particle Size:  $1.10~\mu$  .

-61-

## TABLE XXVII

		1.86	190	187	211	217	
OMPOSITION BY/WI	<u>r.                                    </u>			Actual Wt.	•		
arbon ACC - Pe	troleum Coke Based	480 g	480 g	470 g	470 g	380 g	
Thixotrope	(1) Bentonite	9 9	9 g	9 g	9 g	. 9 g	
	(2)						
-	(3)						~
_	(4)				<del></del>	<b></b>	
Dispersant	(1) Darvan No. 2	24 g	24 g	24 g	24 g	24 g	
J. Jper Juill	(2)	-7 Y	-7 9	27 9	£7 y	9	
_	(3)	†	<del></del>				
	(4)						
Pioment '	1100 Yellow	60 g	60 g	68 g	68 g	68 g	
	Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 q	6 0				
-	(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>			6 9	6 q	6 6	
olvent, Water/A	lcohol 60/40 By Vol.	756	756	756	756	756	
<del></del>	: Homogenizer, Minutes	30	60	30	30		
CHARACTERISTICS							:
Viscos	ity, CP	<del></del>	· · · · · · · · · · · · · · · · · · ·				
<u>Viscos</u> : Imed.	ity, CP Helipath "C"	9,000	8,000	6,000	6,000	2,500	
Imed. After		9,000		6,000	6,000 4,000	2,500	
Imed.	Helipath "C"		5,250				
Imed. After	Helipath "C" #4 @ 10 RPM	5,250 3,225	5,250	3,900 2,400	4,000 2,350	1,425	
Imed. After Mix After 24	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM	5,250 3,225 4,000	5,250 3,200	3,900 2,400	4,000 2,350	1,425 - 850	
Imed. After Mix After	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM	5,250 3,225 4,000	5,250 3,200 •4,500 2,700	3,900 2,400 6,000	4,000 2,350 6,000	1,425 850 2,500	
Imed. After Mix After 24 Hours	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C"	5,250 3,225 4,000 2,300 1,500	5,250 3,200 •4,500 2,700 1,800 2,000	3,900 2,400 6,000 4,000 2,300 6,000	4,000 2,350 6,000 3,900 2,300 6,000	1,425 850 2,500 1,400 850 1,900	
Imed. After Mix After 24 Hours After 7	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM	5,250 3,225 4,000 2,300 1,500 1,100	5,250 3,200 •4,500 2,700 1,800 2,000 1,500	3,900 2,400 6,000 4,000 2,300 6,000 4,500	4,000 2,350 6,000 3,900 2,300 6,000 3,850	1,425 850 2,500 1,400 850 1,900 1,000	
Imed. After Mix After 24 Hours	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM	5,250 3,225 4,000 2,300 1,500 1,100 850	5,250 3,200 •4,500 2,700 1,800 2,000 1,500 1,100	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300	1,425 -850 2,500 1,400 850 1,900 1,000 600	
Imed. After Mix  After 24 Hours  After 7 Days	Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"	5,250 3,225 4,000 2,300 1,500 1,100 850 1,000	5,250 3,200 •4,500 2,700 1,800 2,000 1,500 1,100	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750 6,000	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300 5,500	1,425 850 2,500 1,400 850 1,900 1,000 600 1,900	
Imed. After Mix  After 24 Hours  After 7 Days  After 14	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C"	5,250 3,225 4,000 2,300 1,500 1,100 850 1,000 850	5,250 3,200 •4,500 2,700 1,800 2,000 1,500 1,100	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750 6,000 4,400	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300 5,500 3,700	1,425 850 2,500 1,400 850 1,900 1,000 600 1,900 1,000	
Imed. After Mix  After 24 Hours  After 7 Days	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM	5,250 3,225 4,000 2,300 1,500 1,100 850 1,000 850 700	5,250 3,200 -4,500 2,700 1,800 2,000 1,500 1,100 1,500 1,100 900	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750 6,000 4,400 2,725	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300 5,500	1,425 850 2,500 1,400 850 1,900 1,000 600 1,900	
Imed. After Mix  After 24 Hours  After 7 Days  After 14 Days	Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  Helipath "C"  #4 @ 10 RPM  #4 @ 20 RPM  Helipath "C"  #4 @ 10 RPM  Helipath "C"  #4 @ 20 RPM  Helipath "C"	5,250 3,225 4,000 2,300 1,500 1,100 850 1,000 850 700 1,000	5,250 3,200 -4,500 2,700 1,800 2,000 1,500 1,100 1,500 1,100 900 1,500	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750 6,000 4,400 2,725 6,000	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300 5,500 3,700	1,425 850 2,500 1,400 850 1,900 1,000 600 1,900 1,000	
Imed. After Mix  After 24 Hours  After 7 Days	Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM #4 @ 20 RPM Helipath "C" #4 @ 10 RPM	5,250 3,225 4,000 2,300 1,500 1,100 850 1,000 850 700	5,250 3,200 -4,500 2,700 1,800 2,000 1,500 1,100 1,500 1,100 900	3,900 2,400 6,000 4,000 2,300 6,000 4,500 2,750 6,000 4,400 2,725	4,000 2,350 6,000 3,900 2,300 6,000 3,850 2,300 5,500 3,700	1,425 850 2,500 1,400 850 1,900 1,000 600 1,900 1,000	

Particle Size: 1.10 µ

#### (4) <u>UU Carbon - Coconut Shell Based</u>

The coconut shell based carbon used for this evaluation was supplied by Barnebey-Cheney Company in 50 x 200 mesh size particles. The pH value measured 10.4 in aqueous solution. The surface area is 14-16,000 square meters/gram with a  $CCL_4$  activity of 100%.

In order to perform the required number of experiments, a 50 pound batch of UU was ball milled for 16 hours. The average particle size as measured by the Sub-Sieve Analyzer was 0.7  $\mu$ . This carbon was used to prepare suspension for testing bentonite, asbestos, pyrogenic silica and nylon thixotropic agents. As the data in Table XXVIII shows, bentonite gave the highest viscosities and is considered to be the most efficient. In considering particle size and their effect on viscosities, experiments 100 and 129 show that it is possible to attain a much higher carbon loading with 1.2  $\mu$  than 0.7  $\mu$ . Also, the viscosity of the slurry containing the 1.2  $\mu$  is lower and more stable than the one containing the 0.7  $\mu$  carbon. Additional UU carbon was milled to the desired 1-2  $\mu$  particle size and used in making final selection of materials.

In evaluating the coconut shell based carbon with each of the candidate thixotropic agents, formulations were prepared as shown in Table XXVIII. As can be seen by comparing the five experiments, the bentonite thickening agent proved superior to the others tested.

The stability of all the thixotropes did not vary appreciably as can be seen by Experiments 100, 130, 131 and 132. Also as shown by the viscosity reading taken on Formulation Number 129, carbon particle size has a major effect on the stability as measured by viscosity.

In considering the primary objective of obtaining the highest viscosity with the least amount of thixotropic agent, the bentonite appears to be superior to the others tested.

With bentonite being the most efficient thixotrope with the UU carbon, suspensions were prepared to evaluate each of the dispersants. Experiments 129, 138, 139, and 140 shown in Table XXIX give the results of this evaluation. Using a carbon loading of 32.2% (particle size 0.7  $\mu$ ) in each experiment, Marasperse CB appeared to give a better dispersion of carbon particles indicated by the low viscosity. Considering the effect of particle size on percent carbon loading, viscosity and stability, this series of experiments performed to select the most efficient dispersant was repeated using UU carbon with a particle size in the 1-2  $\mu$  range.

A 25 pound batch of UU carbon was pulverized using the Mikro-Pulverizer and then ball milled for 4-1/2 hours. The average particle size was measured by the Sub-Sieve Analyzer with 1.50  $\mu$ . Having selected bentonite as the most efficient thixotrope, suspensions were prepared to evaluate the dispersants. Here again as Table XXX shows, the Nopcosant K dispersant gave unsatisfactory dispersions and was eliminated from further study. Experiment 161, 164, 165, 166, 170 and 171, listed in Table XXIX show Darvan No. 2 to be the most efficient dispersant. Using a carbon loading of 31% (particle size 1.50  $\mu$ ) Darvan No. 2 appeared to give the best dispersion with the lowest viscosity.

Experiments 166, 170 and 171 using a concentration of 2% Darvan No. 2, show that a maximum carbon loading of 34.8% is possible for this particular dispersant.

After selecting Darvan No. 2 as the dispersing agent with UU carbon, the optimum percentage of this dispersant was next evaluated and is shown in Table XXXI. As this series of experiments show, additional amounts of dispersant over 2% had very little effect on viscosities. These results are also shown in Figure 6.

Experiments shown in Table XXXII were conducted to evaluate sodium chromate and sodium silicate as corrison inhibitors. By comparing Experiments 170 and 179 it can be seen that suspensions prepared with sodium silicate had much higher viscosities than did the slurries containing sodium chromate with only slight increase in pH value. Sodium chromate was selected as the corrosion inhibitor.

The effect of mixing time was next evaluated using a 2% concentration of Darvan No. 2 dispersant. Results listed in Table XXXIII show that increases in mixing time give corresponding increase in viscosity. It appears that a

mix time of sixty (60) minutes will be sufficient to provide a uniform slurry that will form a gel-like structure after 24 hours and will hold the 34.8% carbon in suspension.

Table XXXIV show results of evaluating various pigments to produce an olive green. Concentrations up to  $\sim 5\%$  (4.95%) of the Mapico 1100 yellow gave the desired olive green.

Although suspensions containing 34.68% UU carbon have been prepared and are sprayable, stabilization of viscosity during storage remains a problem. Unlike the CWS, where the viscosity tends to raise during storage, the UU suspensions show a sharp decrease during the first 24 hours after mix and continues to drop during storage. Although the thixotropic gel will hold the carbon in suspension and is stable from that standpoint, attempts to stabilize the viscosity over 30 days and longer storage were unsuccessful.

The optimum formulation for the UU coconut shell based carbon is made as follows:

Ingredient	Actual <u>Weight</u>	Percent Formula Wt.
Carbon: UU	455 g	34.68
Thixotrope: Bentonite	6 g	.46
Dispersant: Darvan No. 2	24 g	1.83
Pigment: 1100 Yellow	65 g	4.95
Corrosion Inhibitor: Sodium	•	
Chromate	6 g	.46
Mix Time: Sixty (60) minutes usin Laboratory Homogenizer		
Typical Viscosity at 24 hours	8,000 cr	s Helipath
after mixing		s #4 @ 10 RPM
•	3,450 c	s #4 @ 20 RPM
pH Value	9.6	
Carbon Particle Size	1.5 µ (a	ivg.)

#### TABLE XXVIII

UU	CARBON .	- THIXOT	ROPE EVA	LUATION		<del>,                                     </del>	
FORMULATION NO.	100	129	130	131	132		
COMPOSITION BY/WT.			. Ac	: :tual Wt.			
Carbon UU - Coconut Shell Based	400 <sup>1</sup> g	350 <sup>2</sup> g	350 <sup>2</sup> g	350 <sup>2</sup> g	350 <sup>2</sup> g		
Thixotrope (1) Bentonite	6 g	6 g	·				
(2) RG-244	<u> </u>		6 g				
(3) COK-84				6 g			
(4) Ny lon-6					6 g		
Dispersant (1) DAXAD 11	12 g						
(2) Darvan No. 2							
(3) Marasperse CB							
(4) Nopcosant K							
Pigment 1100 Yellow	60 g						
Corrosive Inhibitor (1) Na C O	6 g	6 g	6 g	6 g	6 9		
(2) Na S.O.							
Solvent, Water/Alcohol 60/40 By Vol.	756 ML						
MIXING TECHNIQUE: Homogenizer, min.	30	30	30	30	30		

#### CHARACTERISTICS

V1s cos1	ty. O						 <del>,</del> .	<del></del>
Imed.	Helipath "C"	17,000	18,000	15,200	13,000	11,000	<u> </u>	<u> </u>
After	#4 9 10 RPM	13,500	16,200	14,800	12,900	10,800		
Mix.	#4 @ 20 RPM	6,900	8,400	7,900	6,450	5,525		
After	Helipath "C"	15,000	21,500	19,000	16,000	13,700		
24	#4 @ 10 RPM	10,800	19,300	17,800	15,500	13,000		
Hours	#4 @ 20 RPM	5,650	9,350	9,400	7,800	6,800		
After	Helipath "C"	18,000	28,000	18,800	21,000	14,000		
7	#4 @ 10 RPM	14,400	22,400	17,550	18,300	13,800		
Days	#4 @ 20 RPM	7,400	11,700	9,350	9,450	7,225		
After	Helipath "C"	20,000	33,000	18,000	21,000	13,000		
14	#4 @ 10 RPM	15,000	25,400	16,900	16,000	12,900		
Days	44 0 20 RPM	7.775	13,250	8,950	8,800	6,750		
	Helipath "C"	22,000	41,000	17,000	23,000	13,000		
After 30	#4 0 10 RPM	18,400	28,400	16,500	14,100	12,700		
Days	#4 @ 20 RPM	9,500	15,200	8,900	9,000	6,550		
рH		10.2	9.4	9.6	9.6	9.6		

<sup>1.</sup> Ball mill 64 hours - Particle Size Average 1.2  $\mu$  - 1-2 lb batch size 2. Ball mill 16 hours - Particle Size Average 0.7  $\mu$  - 50 lb batch size

#### TABLE XXIX

		•••	/////	•					
	uı	J CARBON	- DISPE	RSANT EV	ALUATION	1			
FORMULATION NO.		129	138	139	140				<u> </u>
COMPOSITION BY/WT	T.			. A	ctual Wt	•			
Carbon UU - Coc	onut Shell Based	350 g	350 g	350 g	350 g	<u></u>			
Thixotrope	(1) Bentonite	6 g	6 g	6 g	6 g			_	
	(2)								
_	(3)							-	
·	(4)								
Dispersant	(1) DAXAD 11	12 g							
<b>-</b>	(2) Marasperse CB		12 g						
-	(3) Darvan No. 2			12 g			<b></b>	<del></del>	_
(4) Nopcosant K					12 g	<b></b>			
Pigment 1100 Yellow		60 g	60 g	60 g	60 g		<del></del>		
Corrosive Inhibitor (1) Na C O.		6 g	<u>6 g</u>	6 g	6 9			ļ	
(2)		4					<del></del>	<b>_</b>	<b></b>
Solvent, Water/Alcohol 60/40 By Vol.		756 ML		756 ML			<del>                                     </del>	<del>                                     </del>	
MIXING TECHNIQUE	: Homogenizer, min.	30	30	30	30				<u></u>
CHARACTERISTICS									
Viscos	ity, C		·		r	·	<del></del>		<b></b>
Imed.	Helipath "C"	18,000	4,000	8,700	35,000			-	
After	#4 0.10 RPM	16,200	2,800	7,300	29,000		ļ		L
Mix	#4 0 20 RPM	8,400	1,500	3,900	14,900		<u> </u>		
After	Helipath "C"	21,500	3,500	6,000	29,000				
24	#4 @ 10 RPM	19,300	1,800		19,700				
Hours	#4 @ 20 RPM	9,350	1,000		12,900				
After	Helipath "C"	28,000	2,500	4,000	21,500				
7	#4 0 10 RPM	22,400	1,500	3,000	18,000				
Days	#4 0 20 RPM	11,700	850	1,600	10,600				
After	Helipath "C"	33,000	3,400	4,000	19,000				
14	#4 0 10 RPM	25,400	1,600	2,700	16,500				
Days	#4 @ 20 RPM	13,250	950	1,475	9,500				
		1					7	<b>—————————————————————————————————————</b>	_

pН

After 30

Days

Helipath "C"

#4 @ 10 RPM

#4 @ 20 RPM

5,000

2,000

1,150

9.4

AND THE PROPERTY OF THE PARTY O

4,900 17,000

2,700 16,400

8,950

9.8

1,500

9.5

41,000

28,400

15,200

9.4

## TABLE XXX

UU CARBON - DISPERSANT EVALUATION										
FORMULATION NO.		164	165		166	170	171			
COMPOSITION BY/WT.			Ac	tual Wt.	, ,.					
Carbon UU - Coconut Shell Based		385 g	385 g		400 g	455 g	455 g			
Thixotrope (1) Bentonite	6 g	6 g	6 g	(40)	6 g	6 g	6 g	! ! •		
(2)				ı ö			-	   \\ \\ \\ \		
(3)	:			ted						
(4)			u	iminate Formul						
Dispersant (1) DAXAD 11	12 g							<del>-</del>		
(2) Darvan No. 2		12 g		Ref	24 g	24 g				
(3) Marasperse CB	-		12 g				24 g			
(4) Nopcosant K	-			- E -	·					
Pigment 1100 Yellow	60 g	60 g	60 g		60 g	60 g	60 g			
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 g		6 g	6 g	6 g			
(2)	<u> </u>									
Solvent, Water/Alcohol 60/40 By Vol., ml		756	756		756	756	756			
MIXING TECHNIQUE: Homogenizer, minutes	30	30	30		30	30	30			

## CHARACTERISTICS

Viscos	ity, CP		, <u>-</u>		,	<del></del>	, 1 <del></del>	, <u>-</u>
Imed.	Helipath "C"	12,000	8,500	9,000	6,000	13,000	19,000	L
After Mix	#4 @ 10 RPM	9,400	5,600	6,600	3,825	9,400	14,300	] ∔ •
	#4 @ 20 RPM	4,800	2,950	3,400	2,075	5,150	7,400	Ĺ
After	Helipath "C"	14,000	4,000	7,000	2,300	3.500	5.000	
24	#4 @ 10 RPM	9,900	2,600	4,500	1,450	1,900	2,600	
Hours	#4 @ 20 RPM	5,175	1,475	2,400	850	1,275	1,675	
After	Telipath "C"	26,000	3,700	5,000	400	1,200	2,000	<u> </u>
7	#4 @ 10 RPM	16,200	2,100	2,200	300	850	1,300	
Days	#4 @ 20 RPM	8,550	1,200	1.300	225	625	900	<u>.</u>
After	Helipath "C"	31,000	5,000	4,500		800		
14	#4 @ 10 RPM	19,000	2,800	2,000	]ed	550	700	
Days	#4 @ 20 RPM	10,000	1,600	1,150	ett	475	600	
A.C.A	Helipath "C"	44,000	9,000	3,500		500	600	
After 30	#4 ७ 10 RPM	22,000	4,600	1,800		450	500	
Days	#4 ७ 20 RPM	13,600	2,500	1,175		425	400	
_рн	-	9.6	9.6	9.6	9.5	9.5	9.7	

Particle Size: 1.50 μ

#### TABLE XXXI

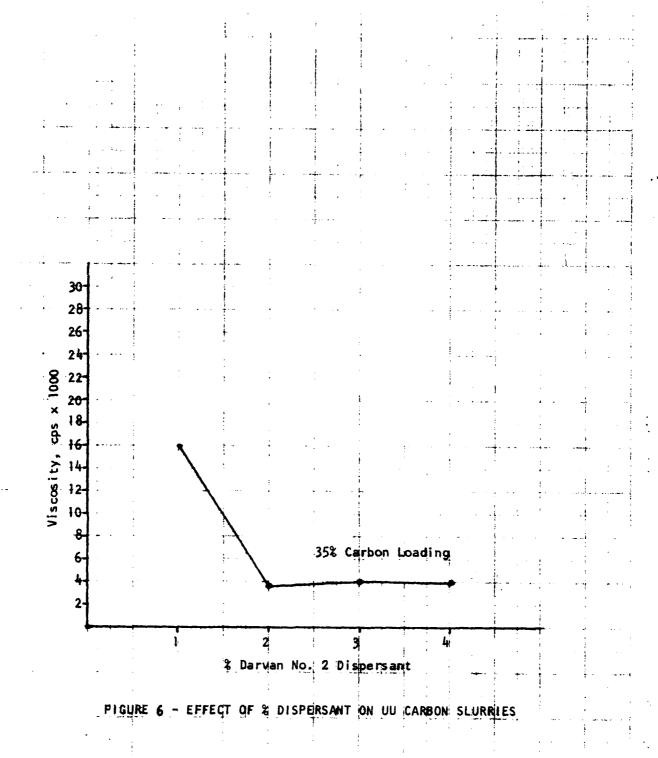
UU CARBON - PERCENT DISPERSANT EVALUATION									
FORMULATION NO.	173	170	174	175					
COMPOSITION BY/WT.			Actual Wt.		' ! ! !				
Carbon UU - Coconut Shell Based		455 g	455 g 455 g		<u> </u>				
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g			-		
. (2)							V		
(3)									
Dispersant (1) Darvan No. 2 (2)	12 g	24 g	36 g	48 g					
(3)									
(4)	-				·				
Pigment 1100 Yellow	60 g	60 q	60 g	60 g					
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 q	6 g	6 g					
(2)	1								
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756	756	.		. 🕳		
MIXING TECHNIQUE: Homogenizer, minutes	30	30	30	30			~ <b>-</b>		

CHA	DΛ	CT	E D	TC	TI	27
CHA	$\sim$	C I		10		C.J

Viscost	ty, CP	market = = = = = = = = = = = = = = = = = = =			, , .	т	r- · ·	1 .	
Imed.	Helipath "C"	28,000	13,000	13,000	14,000				[ }
After Mix	#4 @ 10 RPM	20,000	9,400	8,600	9,250				•
	#4 @ 20 RPM	13,000	5,150	4,750	5,100			CHATTA I PAGE 1 AND	
After	Helipath "C"	16,000	3,500	4,000	3,900				
24	#4 @ 10 RPM	13,200	1,900	2,300	2,300				 
Hours	#4 @ 20 RPM	6,800	1,275	1,450	1,425			<b> </b>	
After	Helipath "C"								<b> </b> <b></b>
7	#4 @ 10- RPM								ļ
Days	#4 @ 20 RPM		···						: 4
After	Helipath "C"								T
14	#4 @ 10 RPM	•				\ <del> </del>			! 
Days	#4 @ 20 RPM								
	Helipath "C"								
After 30 Days	#4 @ 10 RPM	·							
	#4 @ 20 RPM								
рН							1		

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indl'.



# TABLE XXXII

UU CAF	BON - C	ORROSION	INHIBITOR EVALUATION	<del></del>	
FORMULATION NO. ,	1 70	179			
COMPOSITION BY/WT.			Actual Wt.		
Carbon UU - Coconut Shell Based	455 g	455 g			
Thixotrope (1) Bentonite	6 g	6 g	·		
(2)					· •
(3)					
				<u> </u>	
Dispersant (1) Darvan No. 2	24 g	24 g			·
(2)					
(3)					
(4)	ļ				
Pigment 1100 Yellow	60 g	60 g		-	
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g			ļ	<del></del>
(2) Na <sub>2</sub> S <sub>1</sub> O <sub>3</sub>		6 g			
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756			
MIXING TECHNIQUE: Homogenizer, minutes	30	30		<u> </u>	

# CHARACTERISTICS

V1s cos1	ty, '0		<u>,</u>	 	- <del></del>		·	, <u> </u>
Imed.	Helipath "C"	13,000	62,000		<u> </u>	<u> </u>	•	
After	#4 #10 RPM	9,400	21,800	<u> </u>				
Mix.	#4 @ 20 RPM	5,150	13,250		1			
After	Helipath "C"	3,500	54,000					
24	#4 @ 10 RRM	1,900	22,200					
Hours	#4 @ 20 RPM	1,275	12,000					
After	Helipath "C"	1,200						
7	## @ 10 RPM	850						
Days	#4 0 20 RPM	625	A B	 ١.				
After	Helipath "C"	800						
14	#4 0 10 RPM	550						
Days	#4 @ 20 RPM	475						
	Helipath "C"	500		,				
After 30	#4 0 10 RPM	450						
Days	#4' @ 20 RPM	425						
pH		9.5	9.7					

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# TABLE XXXIII

FORMULATION NO.	170	194	195	196	197		ļ
COMPOSITION BY/WT.			Ac	tual Wt.		·	
Carbon UU - Coconut Shell Based	455 g	455 g	455 g	455 g	455 g		
Thixotrope (1) Bentonite	6 g	6 g	6 g	6 g	6 g		
(2)							-
(3)							
(4)							
Dispersant (1) Darvan No. 2	24 g	24 g	24 g	24 g	24 g		
(2)							
(3)				·}			
(4)							L
Pigment   100 Yellow	60 g	60 g	60 g	60 g	60 g		
Corrosive Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 g	6 g	6 g		
(2)							
Solvent, Water/Alcohol 60/40 By Vol., ml	756	756	756	756	756		
MIXING TECHNIQUE: Homogenizer, minutes	30	60	90	120	180		6

# CHARACTERISTIGS

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Viscosi	ty, CP			· .	******		 	<b></b>
Imed.	Helipath "C"	13,000	27,000	21,500	30,000	49,000		
After	#4 @ 10 RPM	9,400	18,800	16,900	22,000	29,000		
Mix	#4 @ 20 RPM	5,150	10,050	9,000	11,800	16,000		
After	Helipath "C"	3,500	9,000	10,000	15,500	24,000		Tr tu
24	#4 @ 10 RPM	1,900	6,900	7,600	11,000	19,800		
Hours	#4 @ 20 RPM	1,275	3,975	4,300	6,200	10,800		
After	Helipath "C"	1,200	5,000	7,000	13,000	20,500		
7	#4 @ 10 RPM	850	3,500	4,700	8,000	15,100		
Days	#4 0 20 RPM	625	2,250	2,950	4,725	8,400		÷.
After	Helipath "C"	800	4,000	6,000	10,000	23,000		
14	#4 0 10 RPM	550	3,000	4,500	7,600	17,400		
Days	#4 @ 20 RPM	475	1,950	2,850	4,600	9,700		
4.54	Helipath "C"	500	5,000	10,000	16,000	34,000		
After 30	#4 @ 10 RPM	450	3,550	6,300	11,500	22,700		
Days	#4 @ 20 RPM	425	2,350	3,900	6,750	12,400		
рН		9.5	9.6	9.6	9.6	9.6		
Solv	vent Content, %	58.9				57.9		

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# TABLE XXXIV

	UU C	ARBON - F	IGMENT	EVALUAT	ON				, ,
FORMULATION NO.		170	203	204	205	<u> </u>	<u> </u>		
COMPOSITION BY/WT	•.			A	' ctual Wt				
					•		<b>F</b>		
	oconut Shell Based	455 g		455 g		1.	<del> </del>		<del> </del>
Thixotrope	(1) Bentonite	6 9	6 g	6 g	6 g	<del> </del>	<b>_</b>	ļ	ļ
٠	(2)			<b>-</b>		<del> </del>	-		785
_	(3)			-		ļ	<u> </u>		
· .	(4)		ļ	<b>-</b>		<b> </b>	ļ		
Pigment	(1) 1100 Yellow	60 g	65 g	<b></b>		ļ	ļ		
-	(2) Cad Yellow/Cad Oran	nge		56/5 g	<del></del>	ļ			
	(3) Azo Yellow	<del></del> -	<b></b>		65 g	<del> </del>	-	,	
	(4) : Darvan No. 2	24 g	24 g	24 g	24 g		<del> </del>		
	Inhibitor (1) Na <sub>2</sub> C <sub>r</sub> O <sub>4</sub>	6 g	6 g	6 g					
001103110	(2)	<del>- 9 9</del>	0 9	1 9	<u>v_</u> g_		-		
Solvent, Water/A	lcohol 60/40 By Vol., m	1 756	756	756	756	1			
MIXING TECHNIQUE	: Homogenizer, Minutes	30	30	30	30				
CHARACTERISTICS Viscos	ity, CP	1	1			<b></b>	Γ	<u> </u>	
Imed.	Helipath "C"		33,000	29,000					
After Mix •	#4 @ 10 RPM #4 @ 20 RPM		11,800	19,800					,
	Helipath "C"		10.000		38,000		-		<b>. 194</b>
After 24	#4 @ 10 RPM	2,300	7,900	6,200	15,400				<b></b>
Hours	#4 @ 20 RPM	1,450	4,550	3,625	7,800				
	Color,	Olive	Olive	Dark					
	Wet	Green	Green	Green	Black				
÷	<del></del>								-
	Color,	Olive	Olive	Dark	D1!				
	Dry	Green	Green	Green	Black			<del> </del>	-
•		+							
		<del></del>						-	
									<del> </del>
		,	,						
pH									

## d. The Formation of Thixotropic Gels

In working with the four different based carbons, it was observed that during the first three days storage of certain carbon slurries, a thixotropic, non-pourable, uniform gel is formed. This is considered a very important and desirable condition in that it prevents the settling out of the carbon particles. It is believed that this gel forms as a result of the interaction of bentonite with the active carbon.

This gel-like structure is very shear sensitive and can be easily made fluid by one or two shakes of the container.

It can be concluded from the data presented in Table XXXV that slurries with high undisturbed viscosities as high as 102,000 centipoise (and possibly higher) can be easily reconstituted into a fluid state with lowered viscosities that can be easily sprayed. For example, Formulation No. 138 with an undisturbed viscosity of 102,000 centipoise reconstitutes easily to 6,000 centipoise.

Of equal importance is the fact that the gel-like structure will reform repeatedly after being reconstituted to the fluid state.

As required by the contract, samples of each of the optimized formulations were submitted to Edgewood Arsenal for evaluation and testing. A "B" portion of each sample was retained at Brunswick to monitor the effect of static storage. Table XXXVI shows the effect of storage up to 142 days. It is felt that, based on this data, storage for 2 years will not adversely effect these carbon loaded thixotropes.

TABLE XXXV

FORMATION OF A THIXOTROPIC GEL

	Notes						Very heavy			Hard gel but	tuted						
Easily	Reconsti- tuted	Yes	<u>8</u>	Yes	8	Yes	8	Yes	Yes	Yes	,		Yes	Yes	Yes	Yes	Yes
	Color	Green	1	Green	Green	Green	Green	Green	Green	Green			Black	Black	Black	Black	Black
Gel	Formation L-M-H(2)	Yes (L)	(H) ON	Yes (M)	(H) ON	Yes (L)	Yes (H)	Yes (M)	Yes (L)	Yes (H)			Yes (L)	Yes (L)	Yes (L)	Yes (L)	Yes (M)
	Amount Settling	0	100%	20%	100%	0	0	0	0	0			0	0	0	0	0
Amount	Free Solvent	20 mJ	100 mJ	82 mJ	ì	23 mJ	6 mJ	3 mJ	8 m]	]] m]			6 mJ	15 mJ	20 mJ	27 m1	9 mJ
Viscosity	Reconstj tution(1)	16,000	1	8,000	1	1,200	3,000	2,000	2,000	34,000			30,000	24,000	14,000	12,000	17,000
Visc	Undist.	70,000	ł	136,000	ł	40,000	>200,000	140,000	74,000	163,000			65,000	28,000	74,000	20,000	70,000
	Form No. CWS Carbon	115	116	711	118	120	137	141	144	145		ACC Carbol <sup>3)</sup>	122	123	124	125	126

TABLE XXXV (Cont'd)

FORMATION OF A THIXOTROPIC GEL

-												<del></del>								
	Notes																			
Easily	Reconsti- tuted	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes		Yes	Yes	No	Yes						
	Color	Green	Green	Green	Green	Green	Green	Green	Green		Green	Green	Green	Green	Green	Green	Green	Green	Green	Green
Gel	Formation L-M-H(2)	Yes (M)	Yes (M)	Yes (M)	Yes (M)	Yes (L)	Yes (L)	Yes (L)	Yes (L)		Yes (L)	(H) ON	(H) ON	Yes (L)						
	Amount Settling	0	0	0	0	0	0	0	0		0	30%	30%	0	0	0	0	0	0	0
Amount	Free Solvent	9 mJ	6 mJ	34 ml	34 ml	39 mJ	21 ml	16 - ա1	18 mJ		7 mJ	62 ml	44 m]	7 mJ	5 mJ	13 ml	2 m]	2 m]	2 m]	6 m
Viscosity	Reconst(1)	30,000	50,000	15,000	27,000	10,000	000*9	5,000	17,500		19,000	11,000	15,000	19,000	9,500	2,000	36,000	28,000	32,000	28,000
Visc	Undist.	>200,000	136,000	110,000	>200,000	100,000	102,000	74,000	82,000		27,000	>200,000	>200,000	44,000	30,000	29,000	000,06	104,000	130,000	108,000
	Form No. UU Carbon	100	129	130	131	132	138	139	140	DARCO KB Carbon	97	104	106	112	113	105	133	136	142	143

<sup>(1)</sup> Reconstituted, Helipath

 $<sup>^{(2)}</sup>$ Light, Medium, Hard  $^{(3)}$ Suspension Prepared with .7  $_{
m L}$  Particle Size Carbon

TABLE XXXVI

STATIC STORAGE TEST OF CARBON THIXOTROPES

	Static	Visc	scosity			(Je)	
	Storage,		Reconstj-,	Free	Amount	Formatjon	Ease of
Form No.	Days	Undist.	tuted(1)	Solvent	Settling	L-M-H(2)	Reconstitution
B-CWS-1	06	180,000	27,000	16.0	0	Σ	Yes
B-ACC-1A	06	120,000	13,500	.5	0		Yes
B-ACC-1B	06	120,000	10,000	7.0	0	۔ ۔	Yes
B-ACC-2	. 06	44,000	3,000	16.0	0	ب.	Yes
B-UU-1	06	200,000+	4,500	10.0	0	Σ	Yes
B-KB-1	06	79,000	7,500	12.0	0		Yes
E-ACC-1-A	142	134,000	14,000	7.0	0	Σ	Yes
E-ACC-2-A	142	51,000	4,000	20.0	0	<b>-</b>	Yes

(1) Reconstituted, Helipath

(2)<sub>Light-Medium-Hard</sub>

## D. Spraying and Adhesion Testing

#### 1. Spray Experiments

To begin spraying experiments with each of the optimized formulations, two 24" x 24" aluminum test panels were spray coated with 1 mil of chromate primer and 1 mil of OG lusterless alkyd lacquer. Test tabs (1 in²) were coated along with the panel and were used for determining the amount of carbon deposited on the surface after each test. The standard U.S. Army sprayer unit equipped with the standard nozzle and .033" diameter atomizing hole was used to test each of the different based carbons. Figure 7 and 8 show the spray set-up and coated test panel.

#### Spray Test No. 1 - CWS Carbon

The optimized formulation as discussed in Section II-C was used for this test. The viscosity measured in the 14,000 centipoise range. The standard sprayer was filled with 1 liter and pressurized to 200 psi from a nitrogen (standard 2500 cubic feet) tank. The 24" x 24" test panel was set 90° to the sprayer nozzle at a distance of 5 feet. One pass was made over the entire panel. As the slurry tends to be broken up into very small droplets, one pass was not sufficient to cover the surface of the panel. Two additional passes were then made which covered the surface completely. After allowing the coating to dry, the test tabs were removed to determine coverage.

Test Tab No.	Carbon Deposited
1	$22.4 \text{ mg/cm}^2$
2	$19.2 \text{ mg/cm}^2$
3	21.9 mg/cm <sup>2</sup>
4	19.6 mg/cm <sup>2</sup>

Because the slurry is being dispensed in very small droplets, requiring 2-3 passes for complete surface coverage, high carbon deposits are being recorded as shown above.

#### Spray Test No. 2 - Darco KB Carbon

The same general procedure was used to test sprayability of the Darco KB suspensions. The viscosity measured in the 17,000 centipoise range. A total of 3 passes was made over the panel with the following coverage:

Test Tab No.	<u>Carbon Deposited</u>
7	$12.6 \text{ mg/cm}_2^2$
2	11.8 mg/cm <sup>2</sup>
3	$10.4 \text{ mg/cm}^2$
4	9.7 mg/cm <sup>2</sup>



FIGURE 7 - SPRAY TESTING APPARATUS TO DETERMINE SPRAYABILITY AND COVERAGE

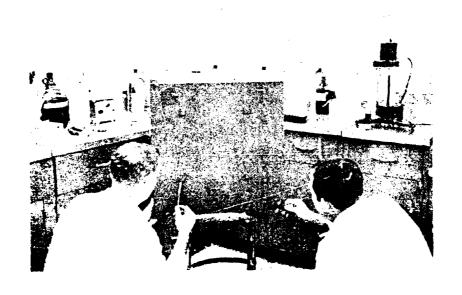


FIGURE 8 - CARBON COATED PANEL WITH TEST TABS TO MEASURE COVERAGE

Again the spray was in the form of very small droplets requiring multiple passes for complete surface coverage.

#### Spray Test No. 3 - ACC Carbon

Although the ACC suspension sprayed better than did the other carbon slurries, the surface coating was similar to that of the previous tests. Again the spray was in the form of small droplets. The viscosity measured in the 6,000 cps range. After 3 passes over the test panel the coverage measured as follows:

<u>Test Tab No.</u>	<u>Carbon Deposited</u>
ו	10.6 mg/cm <sup>2</sup>
2	10.1 mg/cm <sup>2</sup>
3	10.4 mg/cm <sup>2</sup>
4	10.8 mg/cm <sup>2</sup>

The spray tests conducted on the UU suspension gave results very similar to those obtained using the CWS and Darco KB slurries. Each test tab showed an average of 12 mg/cm<sup>2</sup> carbon coating.

By considering stability and sprayability of the different carbon based thixotropes, the suspension prepared with the ACC activated carbon was chosen for additional spray tests.

## Spray Test No. 4 - ACC Carbon

To further test the sprayability of the ACC suspensions, a standard DeVilbiss paint spray gun was used to prepare a test panel. The spray gun was a type MBC with AVI5EX head and DEX needle and was operated at 68 psi air pressure.

From a distance of 15-18 inches, 2 passes were made over the test panel. The resulting spray, fog rather than droplets, gave a uniform even coating. The test tabs were weighed for coverage and the following results were obtained.

<u>Test Tab No.</u>	<u>Carbon</u>	Deposited
1	4.56	mg/cm <sup>2</sup>
2		mg/cm <sup>2</sup>
3		mg/cm <sup>2</sup>
4	3.72	mg/cm <sup>2</sup>

For comparison, a spray test was made with the same ACC suspension but spraying with the standard apparatus. From a distance of 5 feet, operating at 200 psi nitrogen pressure, 3 passes were necessary over the test panel to cover the surface. The test tabs measured the following coverage.

<u>Test Tab No.</u>	<u>Carbon Deposited</u>
ı	8.2 mg/cm <sup>2</sup>
2	$7.8 \text{ mg/cm}^2$
3	9.2 mg/cm <sup>2</sup>
4	8.1 mg/cm <sup>2</sup>

In viewing Figures 9 and 10, it can be seen that a more uniform, even coating is applied using the DeVilbiss gun than was possible with the existing standard spray unit. The panel prepared with the standard apparatus has the larger carbon deposit (8-9 mg/cm²) but has evidence of uncoated areas caused by the droplet form spray.

It can be concluded from the above tests that with some modification to the standard spray apparatus, the ACC carbon slurries can be sprayed satisfactorily to give the desired 3-4  $\rm mg/cm^2$  activated carbon coating.

#### 2. Adhesion Tests

Adhesion tests were next performed using formulations as described in Section II-C. In preparing for abrasion tests, three aluminum panels 3" x 6" were coated with 1 mil of chromate primer and 1 mil of lusterless OG alkyd lacquer. These test panels along with test tabs were then coated with the activated carbon slurry as follows:

Spray Gun: DeVilbiss Type MBC

AV15-EX Nozzle/DEX Needle

Distance: 15-18 inches panel to spray gun

Pressure: 100 pounds air pressure

Passes: 2 in 7-10 seconds

After drying for twelve hours at 72°F and 50% R.H., the test tabs were reweighed to determine coverage. Figures 11 and 12 show the test panel before and after spraying.

Terry cloth strips 3.16 x 3.16 centimeters ( $10 \text{ cm}^2$  surface area) were cut for abrasion pads. A 10 mil thick rigid plastic film was placed over the terry cloth to evenly distribute the 100 gram weight. The weighed terry cloth was dragged over the carbon coating at a rate of 5 inches per minute using the Instron Test Machine (see Figures 13 and 14. The percent carbon loss was calculated as follows:

$$\frac{W_2 - W_1}{P_A} = W_A (gm/cm^2)$$

$$\frac{W_2 - W_3}{T_A} = W_B (g/cm^2)$$

$$\frac{W_B}{W_A}$$
 x 100 = % (g/cm<sup>2</sup>) Carbon Loss

Where:  $W_1$  - Weight of test panel

 $W_2$  = Weight of carbon coated test panel

 $W_A$  = Amount of carbon coating per unit area

 $P_A$  = Area of test panel in cm<sup>2</sup>

 $W_3$  = Weight of test panel after abrasion

 $T_A$  = Area of the abrasion path in cm<sup>2</sup>

 $W_{R}$  = Amount of carbon abraded away

Table XXXVII shows results of the abrasion tests for each of the different based carbons. It can be seen that all carbons are well within the maximum allowable loss of 25%.

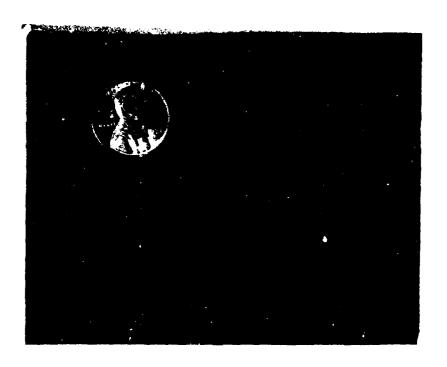


FIGURE 9 - CLOSE-UP OF ACTIVATED CARBON COATING SPRAYED WITH THE STANDARD SPRAYER APPARATUS



FIGURE 10 - CLOSE-UP OF ACTIVATED CAREST COATING SPRAYED WITH A DEVILBISS MBC SPRAY 50%

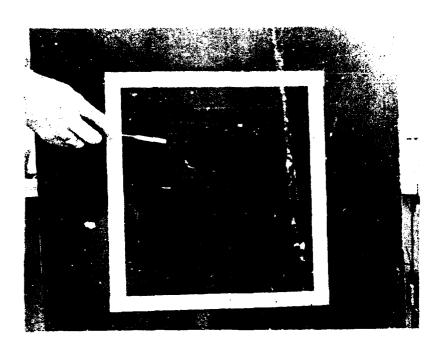


FIGURE 11 CARBON COATED PANEL WITH TEST TABS TO MEASURE COVERAGE

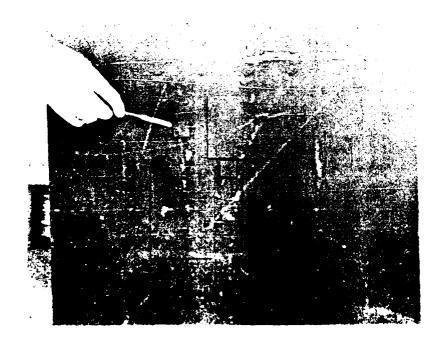
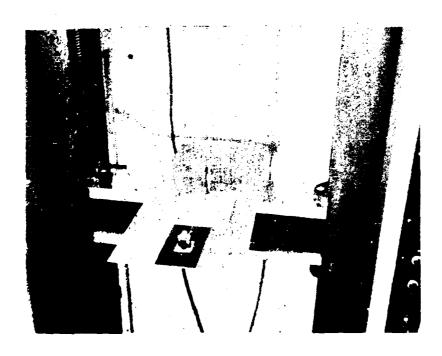


FIGURE 12 ABRASION TEST PANELS WITH A 3-4 mg/cm<sup>2</sup> COATING OF ACTIVATED CARBON



FIGURE 13 ABRASION TEST SET-UP USING INSTRON TEST MACHINE



PIGURE 14 CLOSE-UP SHUMING IUU GKAM WEIGHT AND TERRY CLOTH

TABLE XXXVII

ABRASION RESISTANCE OF ACTIVATED CARBON
DEPOSITED ON ALKYD LACQUER COATED SURFACES

<u>Car</u>	<u>bon</u>	Test Panel Number	Carbon Coating mg/cm <sup>2</sup>	Carbon Loss Percent
1.	CWS	1	3.87	3.30
	Coal Based	2	3.36	6.06
		3	3.55	2.84
2.	Darco KB	10	5.12	4.78
	Wood Based	11	5.49	4.58
		12	4.99	5.18
3.	ACC	7	4.01	6.36
	Petroleum Based	8	4.80	7.19
		9	3.83	6.71
4.	<u>UU</u>	4	3.87	12.09
	Coconut Shell Base	ed 5	3.75	8.92
		6	3.27	6.74

#### III. PHASE B - CLOTHING AND INDIVIDUAL EQUIPMENT DECONTAMINATION

Phase II of the program involves the formulation of dry forms of activated carbon, inert filler and pigment that will give maximum agent vapor absorption when applied onto a surface such as woven uniform fabric material.

Primary objectives are to (1) formulate a dry mixture that will give the highest possible adherence to the surface after some degree of abrasion, and (2) can be easily applied by sprinkling and/or rubbing to give a coating of  $3-4~\text{mg/cm}^2$  of dry activated carbon.

## A. Establishment of Basic Materials, Equipment and Methods of Investigation

Work reported in this report details how selections were made of materials, equipment, and methods of investigation.

## 1. Government Supplied Materials

The following materials were furnished by Edgewood Arsenal as a part of this contract.

Carbon

 Coal based, CWS type manufactured by Pittsburgh Activated Carbon Co.
 The average particle size of the carbon is 1-2 microns.

Uniform Fabric -

Five (5) yard samples of (1) 6 oz. poplin cotton, (2) 8.2 oz. sateen cotton, and (3) 9 oz. Quarpel-treated Nyco sateen uniform material.

#### 2. Inert Filler Materials

The following filler materials were considered for this application.

Asbestos - Samples of each of the two basic types of asbestos were obtained for formulating.

Type I - Serpentine - Grade 4A3, supplied by Van Horn Metz Co.

Type II - Amphibole - Grade 25-PM, supplied by Powhatan Mining Company.

Fibers - Other fibrous materials were also considered.
These include nylon, milled glass and polyethylene.

Pigment - To give an olive green, iron oxide pigment was used.

#### 3. Mixing Techniques and Equipment

Basically, two different mixing techniques were evaluated, i.e., wet and dry. In wet mixing the basic ingredients are combined in an aqueous medium after which it is vacuum filtered and dried. The dry mixing simply involves combining the dry ingredients together by a mechanical mixer. It was the intention of the investigation to establish a method whereby the dry mixing technique will produce a formulation with the same high degree of uniformity as is obtained by wet mixing.

The equipment used in preparation of the carbon formulations was the L-l Laborabory Homogenizer and the Bantam Mikro-Pulverizer. The pulverizer was used to mill the long fiber asbestos (Serpentine) to the desired length as well as preparation of the dry mixes.

## 4. Auxiliary Equipment

Other equipment used in the investigation of these materials included the following:

Applicator Bags - The bags were prepared from cotton knit type fabric and measure approximately 3-1/2" x 6". A nylon scrim "window" was stitched into one side of the applicator and measures 2-1/4" x 4". The "window" is woven with approximately .050" openings between strands and is approximately .010" thick. These applicator bags, along with similar ones supplied by Edgewood, were used to apply a variety of dry carbon mixes to fabric surfaces.

Abrasion Test Apparatus - An abrasion test apparatus was constructed according to the design suggested by Edgewood Arsenal. The apparatus is designed to tumble a carbon loaded woven fabric to simulate the abrading effect resulting from a uniform being worn for a twenty-four (24) hour period. This test machine is described in detail in a later section of this report.

<u>Ball Mill</u> - A two-gallon ball mill was used to tumble selected formulation in an effort to improve the homogeneity. Baffles were later added to the ball mill to improve the mixing effect.

## B. Formulation and Testing of Dry Carbon Mixtures

To begin the investigation of dry forms of activated carbon for an absorbent decontaminant, certain process variables were first established. These process variables include (1) preparation of an asbestos filler prior to the mixing operation, and (2) the effect on the homogeneity of the mixture when prepared in an aqueous medium or simply mixed dry.

The preparation of the filler asbestos (Grade 4A3 - Serpentine) consists of braking up the long fibers into short acicular needles with "exploded" ends to promote both adhesion to woven fabric and entrap the maximum amount of carbon particles. This is accomplished by pulverizing the asbestos through a hammer mill fitted with a fine screen. The size screens evaluated for this application ranged from .010" to .062" openings.

## 1. Microscopic Examination

Samples of the 4A3 asbestos were first prepared (pulverized) for microscopic examination. Glass slides were prepared by mixing small amounts of asbestos in methanol, placing a drop onto the slide and allowing to dry.

Figure 15 shows the long asbestos fibers as received from the Van Horn Metz Company. Figure 16 shows the asbestos after pulverizing through a .010" x .500" slotted screen. It can be seen that the individual fibers are broken up into different lengths ranging from a few microns up to several thousand microns. Figure 17 shows the results of pulverizing the asbestos through a screen having .032" diameter holes. The individual fibers are broken into more uniform lengths than are those put through the .010" x .500" slotted screen. Figure 18 is the result of a screen having .040" diameter holes. As the photograph shows, much longer fibers are getting through the .040" diameter hole than with the previous described screens. Figure 19 is asbestos milled through a screen having .062" diameter openings. As can be seen, only a small percentage of the fibers were broken up into desirable lengths. As the length fibers do not promote sufficient adhesion or entrapment of carbon particles, the .062" perforated screen was eliminated from further evaluation.

Samples of the amphibole type asbestos (shorts) were also examined through the microscope. Figure 20 is a typical example of asbestos "shorts" as received from the supplier. As can be seen, amphibole is composed of approximately 50% fibers and 50% crystalline masses of asbestos. As the fibers provide mechanical adhesion where the crystalline structures will not, it is felt that the amphibole type asbestos does not warrant additional evaluation.



FIGURE 15
CRYSOTILE (TYPE 4A3) ASBESTOS AS RECEIVED FROM VENDOR

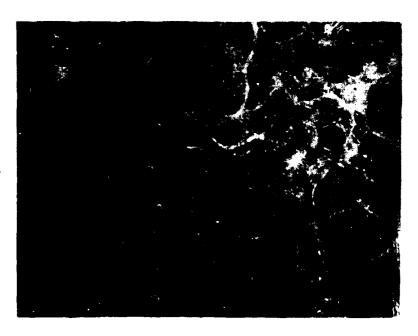


FIGURE 16

4A3 ASBESTOS FIBERS AFTER MILLING THROUGH
A .010" x .500" SLOTTED SCREEN



FIGURE 17

4A3 ASBESTOS FIBERS AFTER MILLING THROUGH
A .032" PERFORATED SCREEN

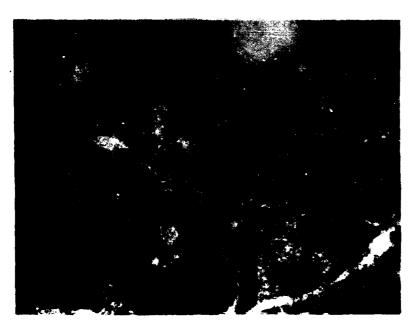


FIGURE 18

4A3 ASBESTOS FIBERS AFTER MILLING THROUGH
A .040" PERFORATED SCREEN

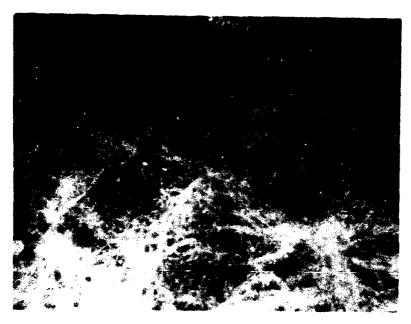


FIGURE 19
4A3 ASBESTOS FIBERS AFTER MILLING THROUGH
A .062" PERFORATED SCREEN

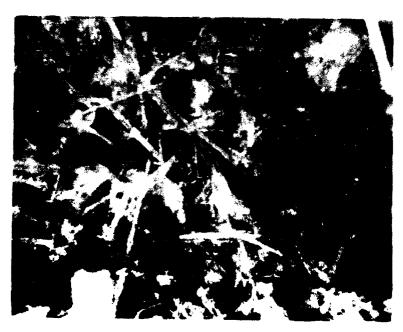


FIGURE 20

AMPHIBOLE TYPE ASBESTOS (SHOR(S))
AS RECEIVED FROM THE SUPPLIER

The two basic types of asbestos discussed above are defined as follows. Type I, Serpentine, (commonly called "crysotile") consists of long flexible fibers composed almost entirely of magnesium silicate. Type II, Amphibole, is a shorter fiber form asbestos, with more brittle fibers composed of various silicates such as magnesium, iron, calcium and sodium. The type is usually referred to as "shorts".

## 2. Preparation of Wet and Dry Formulations

In preparation of the wet mixed formulation, the general procedure was as follows:

Formulation:

1,000 ml of distilled water
5 grams of 4A3 asbestos
100 grams of CWS carbon
10 grams of iron oxide pigment

#### Operations:

The 4A3 asbestos is first milled through the Mikro-Pulverizer to reduce the fiber length. Five (5) grams were then added to the 1000 ml of water and mixed for two (2) minutes with the L-l Laboratory Homogenizer. The 100 grams of CWS carbon and 10 grams of pigment were slowly added and blended for five (5) minutes. The slurry is vacuum filtered and the cake dried for four (4) hours at 220-250°F. The resulting filter cake was broken up using a mortar and pestle and screened through a 40 mesh sieve to give the desired consistency.

In preparing the dry formulations the following general procedure was used.

Formulation:

5 grams of 4A3 asbestos 100 grams of CWS carbon 10 grams of iron oxide pigment

#### Operations:

The 4A3 asbestos was milled the same as for the wet mixes. The asbestos carbon and pigment were then hand mixed with a spatula to distribute the small amount of asbestos throughout the carbon. The mixture was then put through the pulverizer. Some problem was experienced with the separation of the pigment from the mixture by the pulverizer. The dry mixes appeared to contain considerably more carbon dust or "fly" and did not visually appear to be as homogeneous as did the wet mixes. When screened through a 40 mesh sieve, small amounts of asbestos remained on the screen, indicating the

pulverizer did not give sufficient mixing or dispensing of the asbestos throughout the formulation.

To check the uniformity of the mixer, samples were analyzed for variation in particle size using the Sub-Sieve Analyzer. Results show the wet mixes to be very uniform in that particle size did not vary more than .5 microns in the three samples tested, while the dry mixes varied from 1.5 to 10 microns. This would indicate that clusters of asbestos are present.

As a further check to compare the wet and dry mixes, samples of each of the formulations prepared were placed in clean, dry glass containers for dust and adherence tests.

NOTE: This test, suggested by Edgewood Arsenal, is designed to test the amount of dusting (or fly) present in a carbon/asbestos mix, plus any adherence of the mixture to the clean, dry glass wall of the container would indicate a high concentration of the asbestos. After agitation the mixture should be completely settled with 60 seconds with little or no material adhering to the glass walls.

Results of the glass container tests again indicated the wet formulation to be more uniform than were the dry mixes.

#### 3. Abrasion Tests

In order to test the adherence of the carbon/asbestos mixture to woven fabric such as uniform material, a test apparatus was constructed according to the design suggested by Edgewood Arsenal. Figure 21 shows the test apparatus (A) which is designed to tumble the sample holder (B) to which fabric test strips have been attached. Figure 22 is a close-up of the foam cover test cylinder with the fabric samples attached.

The abrasion testing was divided into four basic areas of investigation.

- (1) The effects of wet and dry formulations on the percent carbon retention.
- (2) The effect of formulation moisture content on the percent carbon retention.
- (3) The effect of preparing the asbestos using different screens on the percent carbon retention.
- (4) The percent carbon retention to 6 oz. poplin, 8.2 oz. sateen cotton, and 9 oz. Quarpel-treated Nyco sateen uniform materials.



FIGURE 21
ABRASION TEST APPARATUS

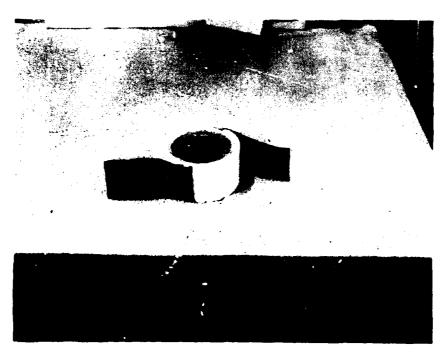


FIGURE 22
FOAM COVERED TEST CYLINDER WITH FABRIC SAMPLES
-95-

## (a) Test Conditions

Cloth strips were tailored to 5.08 x 10.16 cm and impregnated with CWS carbon/asbestos by using a nylon scrim/cotton bag. An average of 8-12 rubs were required to attain the 4 mg/cm coverage. An after-rub with a clean paper tissue was used to remove excess mixture.

As suggested by Edgewood Arsenal, testing was conducted at 20 RPM. However, as can be seen in Test 1, 2, and 3, shown in Table XXXVIII. retention of carbon mixture on the cloth strips after 30 seconds at 20 RPM exceeded 90%. It was concluded from these data that this test was not severe enough to effectively evaluate the four basic areas previously outlined. In order to compare data collected in earlier published work by Edgewood, the conditions were increased to a more severe 65 RPM for 120 seconds.

Tests 4, 5, and 6 were conducted under these conditions with results also shown in Table XXXVIII.

It was then decided to conduct the remaining screening tests at 65 RPM and 120 seconds.

TABLE XXXVIII

PERCENT CARBON RETENTION VS. RPM OF TEST APPARATUS

Test No.	RPM	Test Time, Sec.	Initial Coyerage, mg/cm <sup>2</sup>	Percent Retention
1	20	30	4.7	94.3
2	20	30	3.8	92.4
3	20	30	4.7	90.2
4	65	120	3.9	66.2
5	65	120	3.8	69.0
6	65	120	4.3	66.7

#### NOTES:

- Each of the above values is an average of two (2) samples.
- Tests were performed on 6 oz. poplin material.

## (b) Effects of Wet and Dry Prepared Formulations

Abrasion tests were conducted on formulations as previously described, with the more severe test conditions of 65 RPM for 120 seconds.

As can be seen by the results shown in Table XXXIX, the formulations prepared in the aqueous medium gave the higher retention percentages. This again points up the fact that wet formulations are more uniformly mixed than are the dry formulations.

TABLE XXXIX

PERCENT CARBON RETENTION OF WET AND DRY PREPARED FORMULATIONS AT 65 RPM AND 120 SECONDS ABRASION

Test No.	Initial <u>Coverage</u>	Formulating Condition	Percent Retention
4	3.9	Wet	66.2
5	3.8	Wet	69.0
6	4.3	Wet	66.7
7	4.1	Dry	61.8
8	4.4	Dry	59.6
9	4.2	Dry	59.5

## (c) Effect of Moisture Content

To measure any effect of moisture content of a carbon/asbestos mixture on the percent retention to woven fabric, mixtures were prepared using the wet method. After preparing the formulation a portion was allowed to reach equilibrium at 72°F and 50% R.H. After twelve hours the moisture content measured 1.8%. After 24, 48, and 96 hours the moisture content had stabilized at 2.0%. The moisture content of the CWS carbon, as supplied by Edgewood, is approximately 2.0%.

To obtain the 0.5% moisture, a sample was dried for four (4) hours at 220-250°F. The remaining moisture contents were obtained by adding calculated amounts of water to reach each desired moisture content and allowing approximately 24 hours to reach equilibrium.

Abrasion tests were ten conducted at 65 RPM and 120 seconds as shown in Table XL.

By evaluating this data, it can be concluded that no significant increase in carbon retention results from increasing the percent moisture. The data also shows that approximately 2% water, which is the normal condition of the carbon as received, exhibits good or slightly superior retention.

TABLE XL

# EFFECT OF MOISTURE CONTENT OF A CRABON/ASBESTOS MIXTURE ON THE PERCENT RETENTION TO WOVEN FABRIC

#### 65 RPM and 120 Seconds

Test No.	Initial <u>Coverage</u>	Moisture Content	Percent Retention
5	3.8	.5	67.3
6	4.3	2.0	69.0
12	4.5	7.8	59.2
13	4.4	8.0	66.9
14	4.0	7.8	68.0
15	4.0	12.5	63.5

# (d) <u>Effect of Pulverizing Screen Size</u>

As discussed earlier, samples of crysotile were pulverized through a series of fine screens. To test the effects of different lengths of asbestos fibers on the percent retention to woven fabric, abrasion tests were conducted as shown in Table XLI. In reviewing the data it can be concluded that there was relatively little effect of the fiber length on the retention of the mixture. Fibers ranging from a few microns to several thousand microns are capable of entangling with each other and entrapping carbon particles.

Based on the microscopic examination showing uniformity of the fiber lengths produced by the .032" round screen, it was selected to produce asbestos for the remaining tests.

TABLE XLI

EFFECTS OF PULVERIZING SCREEN SIZE ON PERCENT CARBON RETENTION TO WOVEN FABRIC

Test No.	Initial <u>Coverage</u>	Screen <u>Stze</u>	Percent Retention
16	4.4	.010" x .500" (S)*	64.2
17	4.5	.010" x .500" (S)*	66.3
18	4.5	.010" x .500" (S)*	70.0
4	3.9	.032" (R)*	66.2
5	3.8	.032" (R)*	69.0
6	4.3	.032" (R)*	66.7
19	4.3	.040" (R)*	69.7
20	4.5	.040" (R)*	63.3
21	4.3	.040" (R)*	69.9

NOTE: Formulation prepared as described in Section 2.

Abrasion Tests run at 65 RPM and 120 seconds.

\*(S) = Slotted; (R) = Round

## (e) Effects of Different Types of Woven Fabric

To determine the percent carbon retention on each of the poplin, 6 oz.; cotton sateen, 8.2 oz.; and Quarpel-treated Nyco sateen, 9 oz., uniform fabrics, abrasion tests were conducted and results shown in Table XLII. As tests 24 and 25 show, the Quarpel-treated Nyco sateen retained 77% to 79% after being abraded for 120 seconds at 65 RPM. This is considerably higher than either the 6 oz. poplin or the 8.2 oz. cotton sateen and probably be explained as the difference in weave of the fabric. The Nyco sateen is a much heavier, more coarse fabric which allows more carbon to penetrate into the voids between the individual strands.

Figures 23, 24, and 25 show Quarpel-treated Nyco sateen as received, impregnated with a carbon/asbestos, and after abrasion testing. As can be seen in Figure 24, the mixture covers the entire surface of the fabric at a level of 4 mg/cm<sup>2</sup>. Figure 25 shows the results of abrading for 120

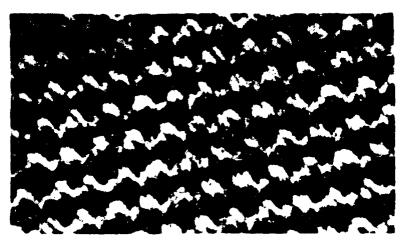


FIGURE 23
QUARPEL-TREATED NYCO SATEEN AS RECEIVED



FIGURE 24

NYCO SATEEN IMPREGNITTO WITH 4 MG/CM<sup>2</sup>
OF CARBON/ASBEST AS MIXTURE

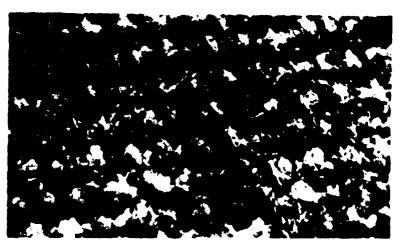


FIGURE 25

NYCO SATEEN AFTER ABRASION TEST
-100-

seconds at 65 RPM. Most of the surface carbon has been removed with the remaining portion being entrapped by a combination of the asbestos fibers and weave voids.

TABLE XLII

PERCENT RETENTION OF CARBON/ASBESTOS
TO DIFFERENT TYPES OF WOVEN UNIFORM FABRIC

Test No.	Initial Type st No. Coverage Fabric		Percent Retention
5	3.8	Poplin. 6 oz.	69.0
6	4.3	Poplin, 6 oz.	66.7
22	4.3	Sateen, 8.2 oz.	58.7
23	4.5	Sateen, 8.2 oz.	61.8
24	4.2	Nyco Sateen, 9 oz.*	77.3
25	4.5	Nyco Sateen, 9 oz.*	78.º

NOTES: Formulation prepared as described in Section 2.

Abrasion test run at 65 RPM and 120 seconds.

\*Quarpel-treated Nyco sateen, 9.0 oz.

## 4. Other Fibrous Fillers

Preliminary evaluation of fibrous materials such as nylon, milled glass and polyethylene was completed. Typical formulation began with 85-90% active carbon, 5-10% pigment and 5% minimum filler. Formulating was conducted using the wet mixing technique as described in Section B-3 of this report.

Samples of the above formulations were submitted to Edgewood Arsenal for evaluation and testing. It was concluded that sufficient work had been completed with fillers to eliminate all but asbestos. At the direction of Edgewood, materials evaluation was limited to asbestos and coal based activated carbon.

## C. Controlling Carbon Flow From Applicator Bags

In order to deposit the desired 4 mg/cm<sup>2</sup> of active carbon onto a surface, using an applicator bag, it would appear desirous to incorporate some type of flow control device. It was considered that by incorporating large open cell polyurethane foam inside the pad the resulting carbon flow could be better controlled to the desired deposition. However, three problem areas appear to prohibit this concept. First, no satisfactory method could be found whereby 120 grams of the carbon/asbestos could be impregnated into the polyurethane foam. Second, by including the foam into the applicator pag, the volume is increased to the point that it will not fit easily into the M-13 container, and third, the polyurethane foam has a tendency to "filter" or separate the asbestos fibers from the activated carbon. It is felt that by adjusting the nylon "window" scrim, the carbon flow during application can be properly controlled. The optimum size, at this point, appears to be 2-1/2" x 4". This allows a 4 mg/cm<sup>2</sup> coverage level to be attained with minimum rubbing.

#### IV. CONCLUSIONS AND RECOMMENDATIONS

Although the water soluble carboxy vinyl polymer thixotropes do provide a stable non-settling, sprayable carbon slurry, gas agent tests have shown that film forming properties adversely effect the important absorptive properties of the activated carbon. Thus, the vinyl polymer system is not suitable for application as a chemical agent decontaminant.

In selecting the optimum ingredients to prepare a stable, sprayable thixotrope that meets all the requirements of the Edgewood specification, the following materials have been shown to be superior.

Coal-based, petroleum-based, coconut shell-based and wood-based carbon all appear to be suitable as gas absorbent decontaminants; however, in considering stability at static storage, the coal-based or the petroleum-based appear to be superior.

Thixotropic additives appear to be limited to the inorganic type with the bentonite showing superior properties to any tested.

Dispersants are effective in lowering the viscosity of a carbon loaded thixotrope, thus allowing the maximum percent carbon loading to retain sprayability. Results show the polymerized salt of alkyl naphthalene sulfonic acid to be best when combined with the coal-based carbon and sodium salts of polymerized substituted benzoid alkyl sulfonic acid to be most effective with the remaining three activated carbon.

Yellow iron oxide pigment, loading to approximately 5% by weight, gives an olive green color when sprayed onto a surface and allowed to dry.

Corrosion and rust can be inhibited by 1/2% by weight of sodium chromate or sodium silicate. Sodium silicate does add to the stability of the petroleum based carbon and is recommended over the sodium chromate with that particular carbon.

A mixture of 40 parts by volume methyl alcohol and 60 parts by volume demineralized water is an effective anti-freeze/carrier system.

The formulation ingredients and composition weights for each of the different based carbons, along with physical characteristics of each, are shown in the formulation and experiments in Section II-C.

In preparing dry powder formulations, Serpentine type asbestos is superior to the Amphibole type in promoting adhesion to woven fabrics.

Formulations prepared in aqueous medium show a higher degree of uniformity than those prepared by simply mixing dry.

Preparation of the asbestos filler can be satisfactorily done by use of a hammer mill fitted with a fine (.032" round holes) screen.

Abrasion tests show active carbon retention to woven fabric to be in the 70% range after a simulated wear of 24 hours.

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The objective of the program was to develop decontaminating systems for persistent chemical agents using micronized carbon. These systems must be effective in absorbing chemical agents and designed to the following goals: (1)

Act rapidly over a wide temperature range,(2)

Be non-toxic and remain stable, (3)

Not damage material and equipment on contact, and (4)

Be easily and rapidly applied to vehicular equipment, clothing and ancillary equipment.

The method of study was to select key ingredients, i.e., activated carbons, thixotropic agents, dispersants, pigments and solvent/antifreeze and formulate a system containing a minimum of 25% active carbon. It should be easily applied by spraying to a coverage of 4 mg/cm² and remain stable (not settle during static storage of at least two years). Key methods of investigation included evaluation of mixing techniques, effects of various thixotropes and dispersant on viscosities and stability and the evaluation of spray equipment for optimization of techniques as well as equipment. In addition, studies were conducted whereby dry formulation of the same key ingredients were formulated using high shear dry mixers. These compounds were tested for uniformity, adhesion to woven surfaces and effective coverages in the

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A mg/cm range.  The results of these studies show that formulations containing approximately 35% active carbon can be easily sprayed to the desired coverage and will remain stable for the desired two year period. All of the program goals outlined above were met or exceeded by this study. Results also show directly formulations can be prepared by a special screened milling process to give the desired uniformity, color and adhesion.  It is concluded that in selecting the optimum ingredients to prepare a stable, sprayable thixotrope that will meet all of the Edgewood requirements, the following materials have shown to be superior: coal, petroleum, coconut and wood based activated carbons are suitable as agent absorbents; however, the coal and petroleum-based appear slightly superior. Thixotropes appear to be limited to the inorganic type with bentonite showing superior thixotropic properties. Dispersants are effective in lowering viscosities with the sodium salts of polymerized substituted benzoid alkyl sulfonic acid being most effective. Color can be obtained with iron oxide and 1/2% sodium chromate or sodium silicate to inhibit rust. A homogenizer mixer will produce uniform mixtures of the wet-system and a special screen milling machine will prepare satisfactory dry formulations.	ROLE		ROLE	WT	POLE	<b>₩</b> ▼	
Activated Carbon Decontaminants Asbestos Adherence Filler Homogenizer Pulverizer Woven Fabric Pigment Thixotropes Dispersants Corrosion Inhibitors Viscosities Slurries							

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